

# TOWARDS MORE EFFICIENT CEMENT INDUSTRIES

ONLINE TECHNICAL WORKSHOP

1 8 0 9 2 3

1 1 : 3 0 TO 1 3  
CEST



## ONLINE TECHNICAL WORKSHOP

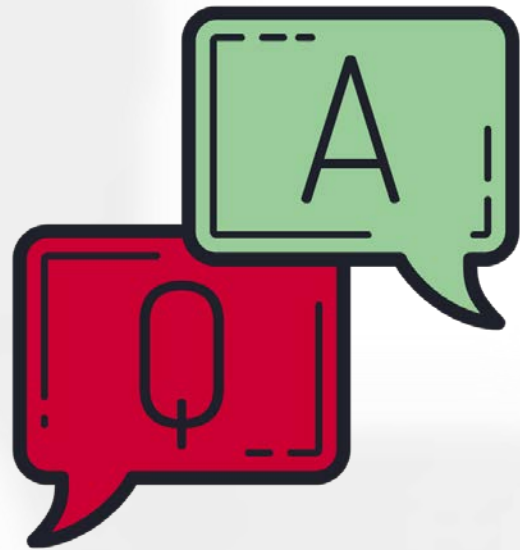


This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 869939.

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# WELCOME!



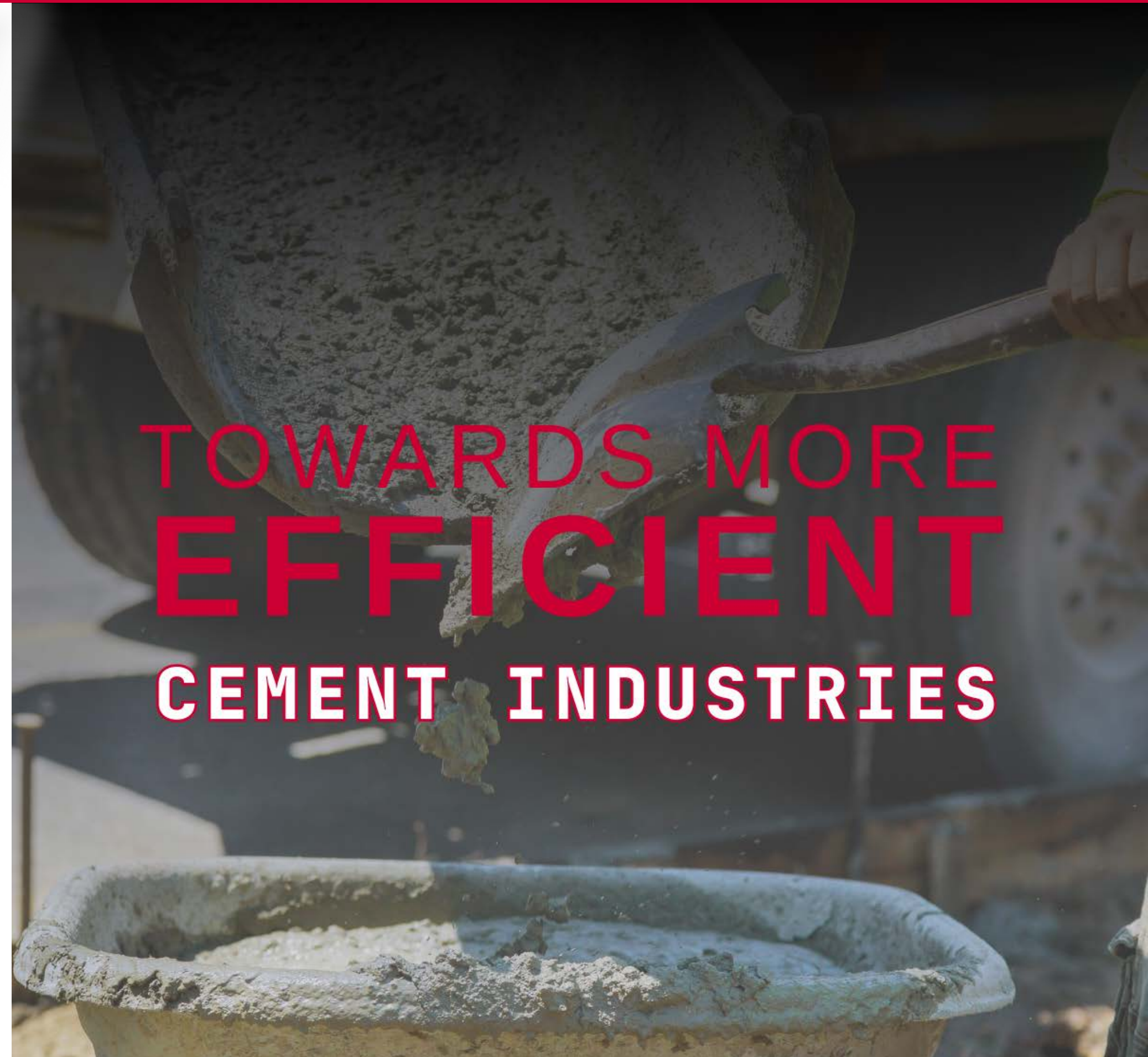
For any question, please type it in the chat.

A dedicated Q&A session is scheduled at the end of the event.



This event is recorded and the video will be publicly stored on the website of the project and within the project consortium.

For more info please visit [www.retrofeed.eu/privacy/](http://www.retrofeed.eu/privacy/)



# Agenda

Monday, 18<sup>th</sup> September 2023

SCHEDULE	AGENDA	SPEAKER
11:15 – 11:30	<i>Reception on MS TEAMS</i>	
11:30 – 11:40	<b>Welcome and RETROFEED introduction</b>	<i>Olga Lysenko (IVL) Roberto Arevalo (CIRCE)</i>
11:40 – 11:55	<b>Digital Twin in cement industry</b>	<i>Antonio Alcaide (CIRCE)</i>
11:55 – 12:10	<b>Flame visualization monitoring tool</b>	<i>Jorge Arroyo (CIRCE)</i>
12:10 – 12:25	<b>Quality measurement monitoring system for clinker</b>	<i>Francisco Rodriguez (AIMEN)</i>
12:25 – 12:35	<b>Main achievements on cement demo site</b>	<i>Valter Tavares (SECIL)</i>
12:35 – 13:00	<b>Q&amp;A</b>	<i>Olga Lysenko (IVL) Diego Redondo (CIRCE)</i>
<b>END OF THE WORKSHOP</b>		



# TOWARDS MORE EFFICIENT CEMENT INDUSTRIES

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**RETROFEED PROJECT**  
**Roberto Arévalo (CIRCE)**



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# Main objective

RETROFEED main objective is to:

**Enable the use of an increasingly variable, bio-based and circular feedstock in process industries through the retrofitting of core equipment, the implementation of an advanced monitoring and control system, and providing support to the plant operators by means of a DSS covering the production chain.**

This approach will be demonstrated in **five Resource and Energy Intensive Industries (REIIs (ceramic, cement, aluminium, steel, and agrochemical)).**



# Overall concept

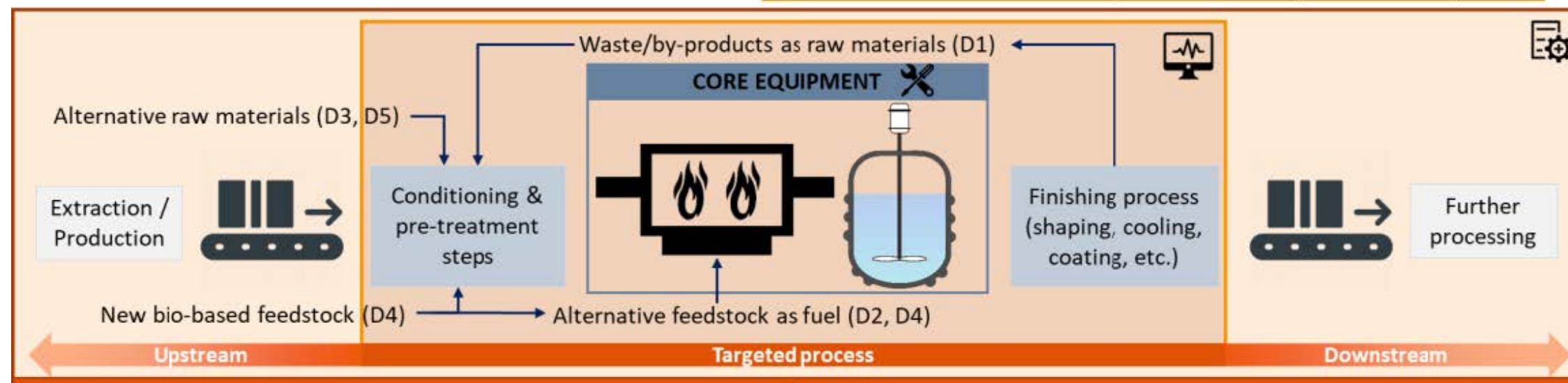


### 1. Ad-hoc retrofitting technologies

Key equipment will be retrofitted through new designs, improved burners, etc. for increasing fuel and raw materials flexibility

### 2. Monitoring and control systems

- Improved sensors for raw material quality and process conditions
- Data processing and analytics for enhancing process monitoring
- Process simulation and techniques for control algorithms development



### 3. Retrofit DSS tool

- Definition of indicators (KRI) for measuring and optimising process performance
- Detection of process inefficiencies and retrofitting potential
- Quantification of the effect of alternative materials in energy consumption and product quality

- ✓ Core equipment retrofitting
- ✓ Improving M&C system
- ✓ Development of new sensors
- ✓ Development of Digital Twins
- ✓ Development of Decision Support Systems
- ✓ TRL 7 solutions





Dá forma às ideias

## CORE EQUIPMENT – ROTARY KILN

### Retrofitting actions

- ✓ Full-scale multi-fuel burner design
- ✓ Image based combustion diagnosis tool
- ✓ Alternative fuels properties determination
- ✓ Real time clinker optical characterization

### Goals

- ✓ CO<sub>2</sub> emissions reduction
- ✓ Replacement of fossil fuel close to 100%
- ✓ Increment in energy efficiency
- ✓ M&C improvement



## CORE EQUIPMENT – MELTING FURNACE

### Retrofitting actions

- ✓ Delacquering system
- ✓ O<sub>2</sub> injection system
- ✓ New burner head design
- ✓ O<sub>2</sub> and TOC analyzers

### Goals

- ✓ 50% increment in the amount of scrap
- ✓ Reduction of the energy consumption 15 times
- ✓ More efficient combustion
- ✓ Reduction of the GHG emissions
- ✓ Improved M&C system

## CORE EQUIPMENT – ELECTRICAL ARC FURNACE



### Retrofitting actions FENO

- ✓ Burner modification for feeding biochar and plastic grains
- ✓ Injection system

### Retrofitting actions SILCOTUB

- ✓ Feeding injection system

### Goals

- ✓ Reduction of GHG emissions
- ✓ Use of alternative feedstock
- ✓ M&C system improvement





## CORE EQUIPMENT – FRITS FURNACE

### Retrofitting actions

- ✓ Feeding system enhancement
- ✓ Redesign of the flue gases recovery system
- ✓ Implementation of new sensors
- ✓ Smart control

### Goals

- ✓ Energy and material savings
- ✓ Optimization use of fuel and combustion air
- ✓ Reduction of material waste
- ✓ Improved M&C system



## CORE EQUIPMENT – PHOSPHOROUS REACTOR



### Retrofitting actions

- ✓ New design of a in-line reactor for alternative phosphorus sources

### Goals

- ✓ Replace 10% of the currently used phosphorous sources
- ✓ Recover valuable raw materials from wastes
- ✓ Reduction of cost
- ✓ M&C system improvement



# Direct impacts

- Increasing the resource and energy efficiency of the targeted processes by 20%;
- Decrease GHG emissions through retrofitting by at least 30%;
- Decreased utilisation of fossil resources in the process industry of at least 20%;
- Reduced OPEX by 30% and increased productivity by 20%;
- Effective dissemination

# TOWARDS MORE EFFICIENT CEMENT INDUSTRIES

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**DIGITAL TWIN IN CEMENT INDUSTRY**  
**Antonio Alcaide (CIRCE)**



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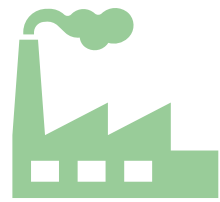
# Digital twin of a cement rotary kiln

## INDEX

1. Context and problem definition
2. Approach and challenges
3. Model development
4. Results from validation and fine-tuning
5. Conclusions

# 1. Context and problem definition

Cement industry pollution



- 5-8 % global CO2 emissions
- Highly energy intensive industry
- Fuels usually account for 30% of total energy consumption
- Alternative fuels allows recycling and provides a solution for avoiding landfill
- Alternative fuels of fossil origin
- Biobased alternative fuels such as wood chips and bone meal, paper, woody biomass
- Refuse Derived Fuels (RDF) from municipal solid waste (cardboard, textiles, fluff...)
- Moisture can range from ~10% to ~30% (up to ~150 mm)
- Heterogeneous mixture of properties, combustion kinetics and high calorific value



Alternative fuels to reduce impact

Use of Refuse Derived Fuel (RDF) and tyres

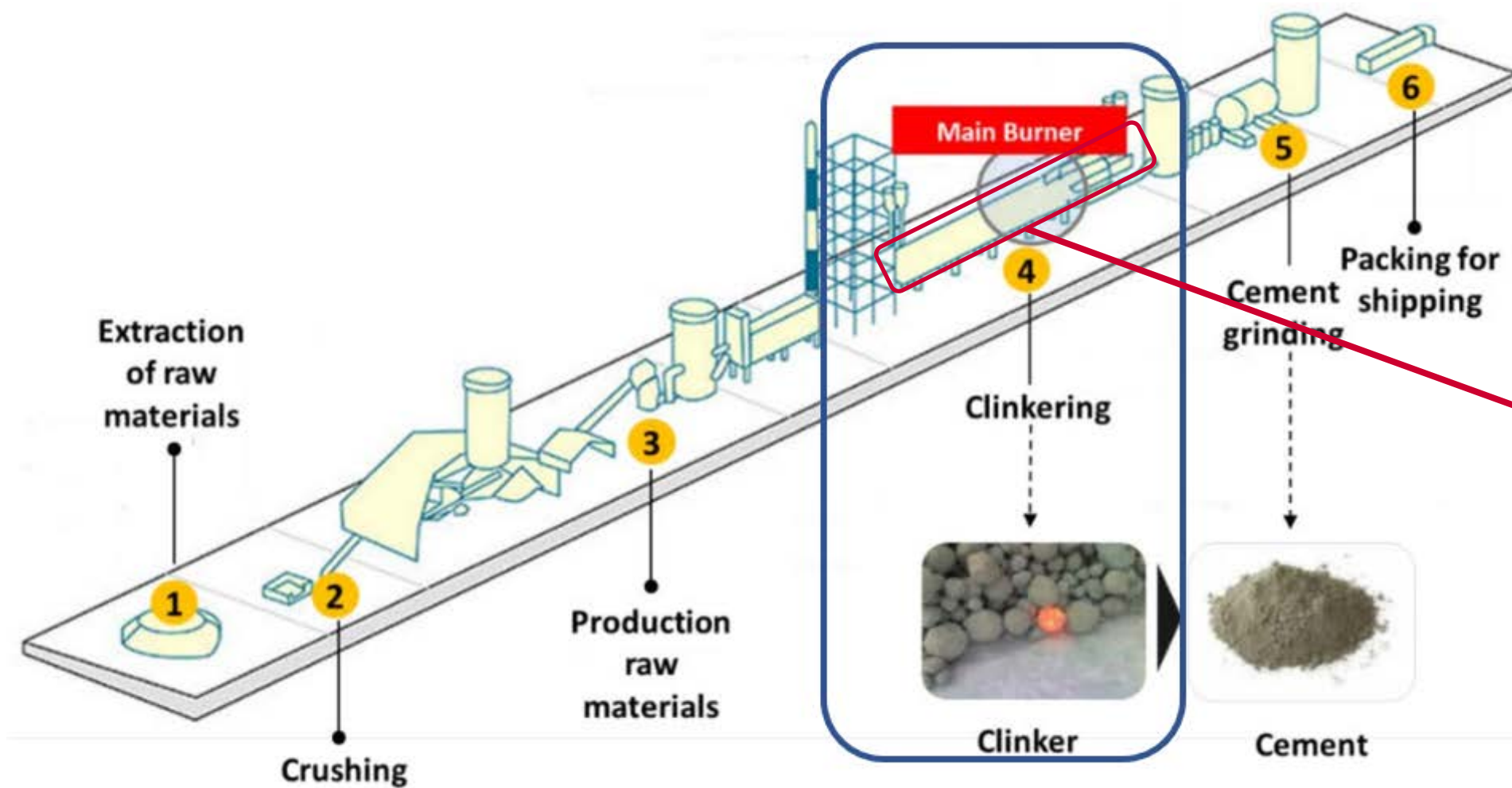
★★★ Low quality fuel (moisture, ashes, big size, heterogeneity)



Complex combustion behaviour



# 1. Context and problem definition



# 1. Approach and challenges

Clinker production requirements



Complex physics inside kiln

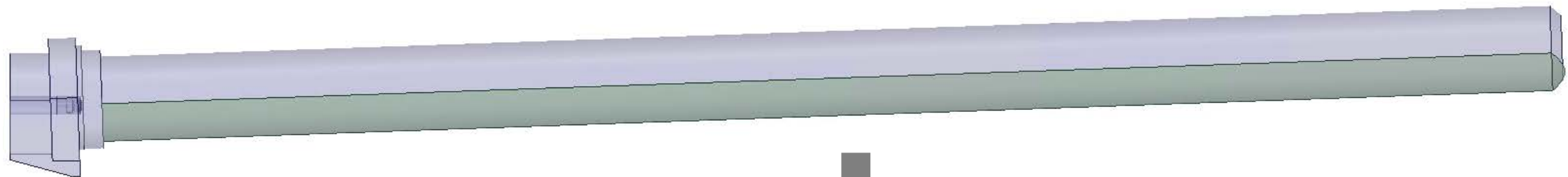


Low quality of RDF

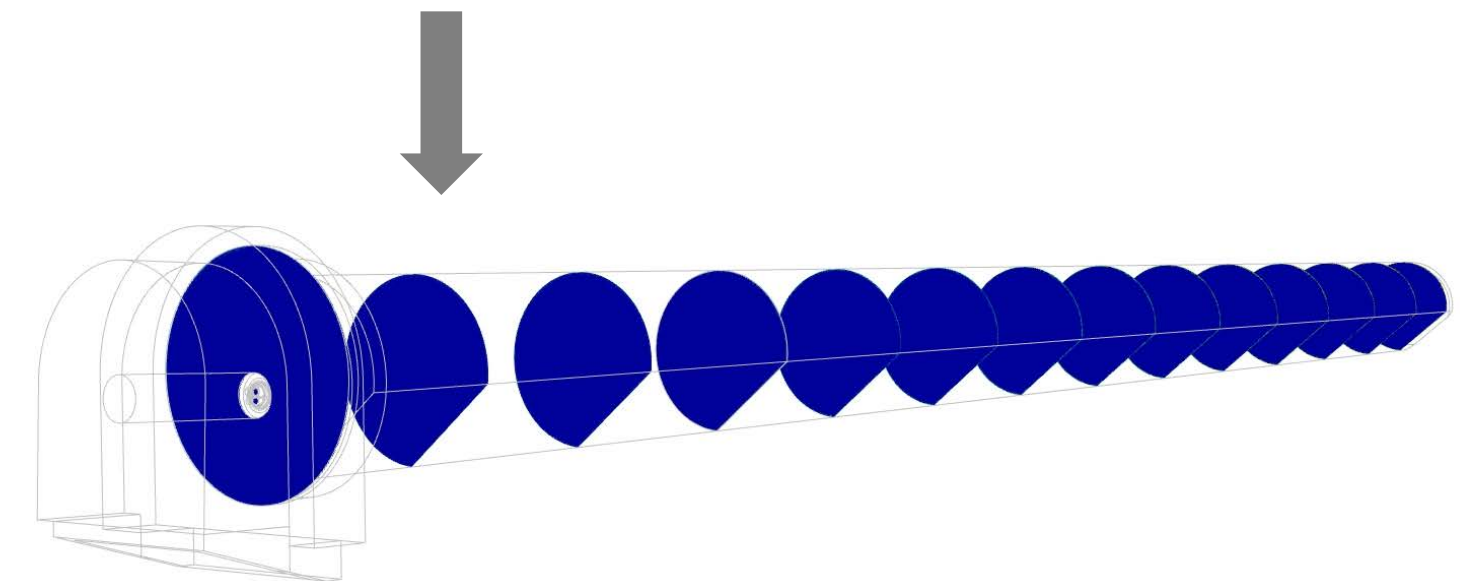
Need of a digital model to assess effect of relevant variables, provide support and test what-if scenarios



CFD model of rotary kiln to solve combustion behaviour of fuels



1D sliced model for solving clinker composition and assessing changes in operational parameters in a computationally cheap way



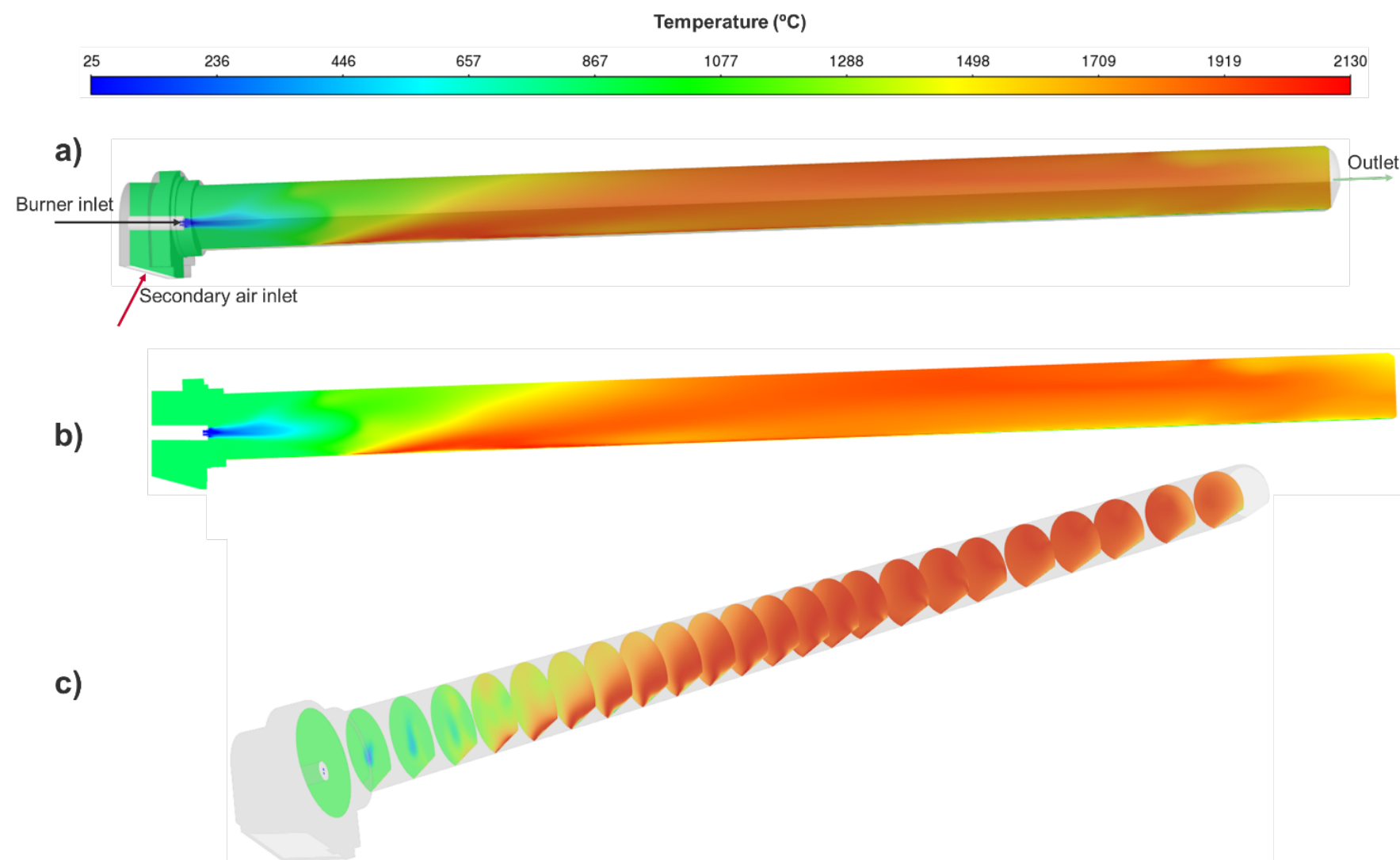


# 1. Approach and challenges

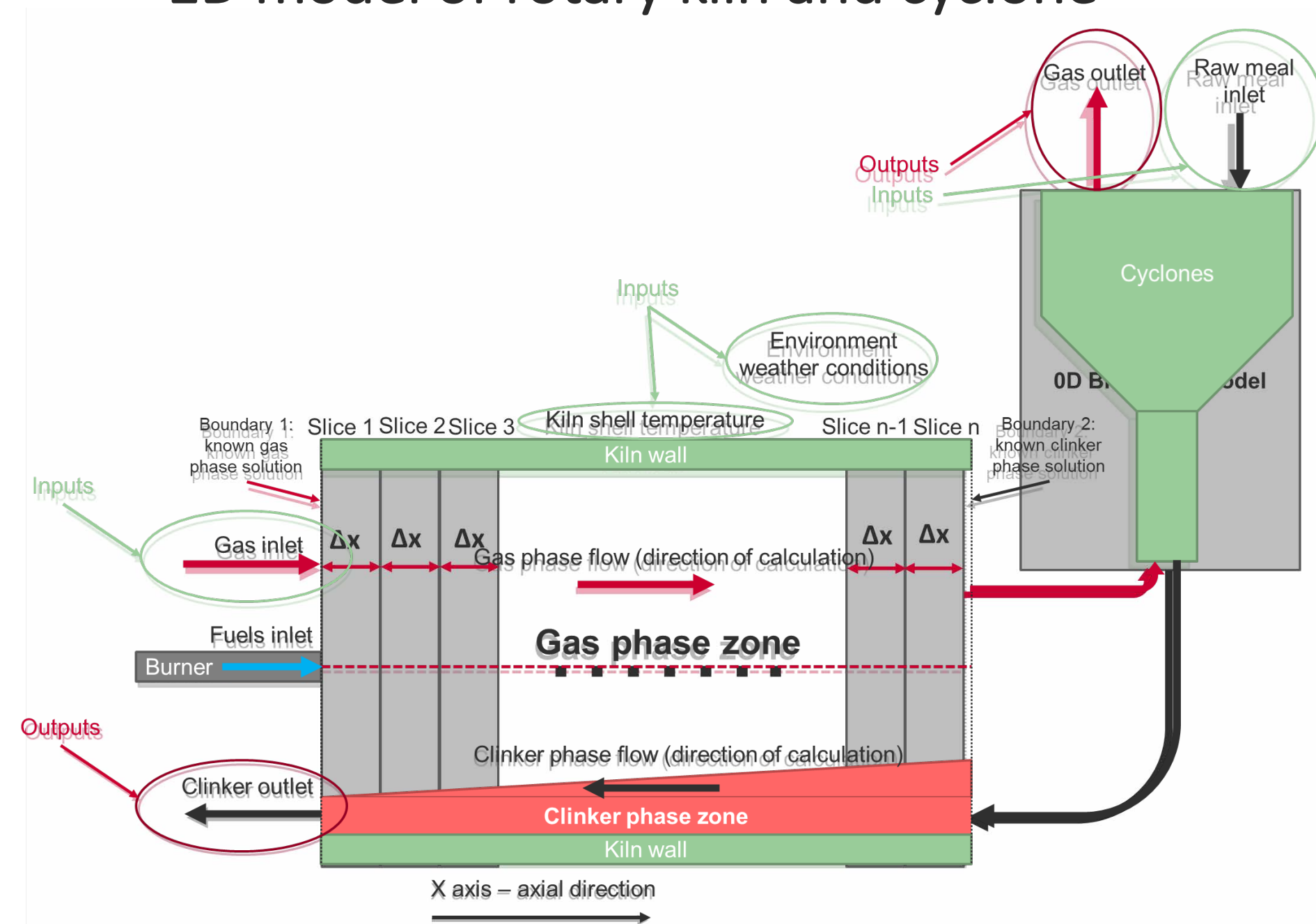
Cause	Problem	Possible solutions	Adopted solution
Local peak values for temperature are not computed	Minor pollutants (NO <sub>x</sub> , SO <sub>x</sub> , CO) formation cannot be considered	Search for simplified models to estimate → Very inaccurate	No minor pollutants will be given as outputs, agreed with partners
Local sinks of oxygen are not computed	All oxygen is available for fuel	Break every slice into different zones to compute location of particle and available oxygen in that location → Difficult, gain in accuracy is not guaranteed	Compute some CFD simulations with representative fuels mixture, and use burning fuels information to feed 1D model as fixed burning values
Flight of particles are not computed	Inaccurate burning location of particles	Perform simplified force balances with empirically obtained correlations to calculate falling locations → Tedious, but possible. Not very accurate	Compute some CFD simulations with representative fuels mixture, and use burning fuels information to feed 1D model as fixed burning values
Heat radiation fluxes are not computed	Inaccurate radiation modelling	Apply direct or network method, using view factors → Possible, but very computationally expensive and complex since it also requires coupling with other heat transfer mechanisms	Use very rough heat transfer contribution estimation, from literature review

# 2. Model development

CFD model of rotary kiln



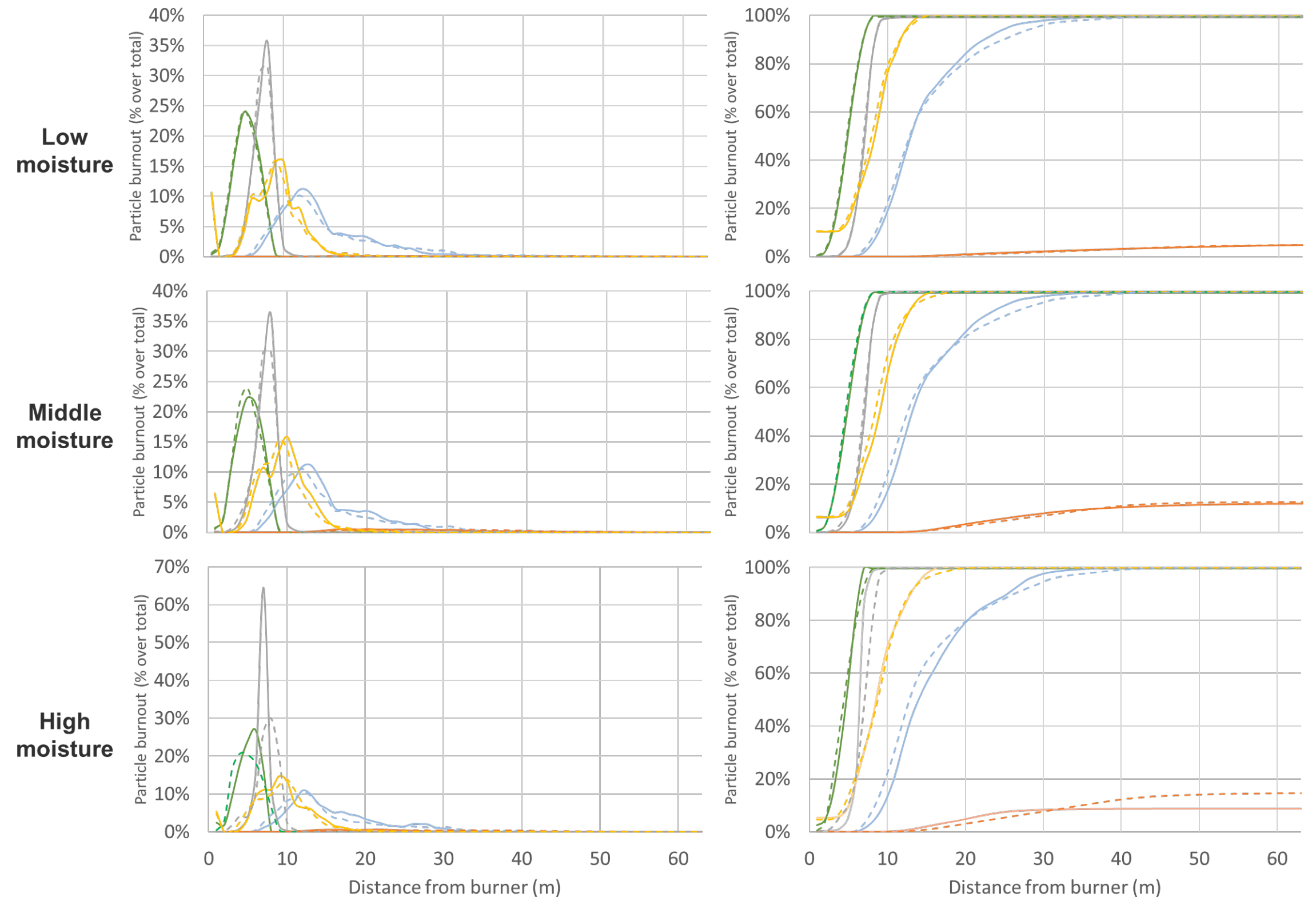
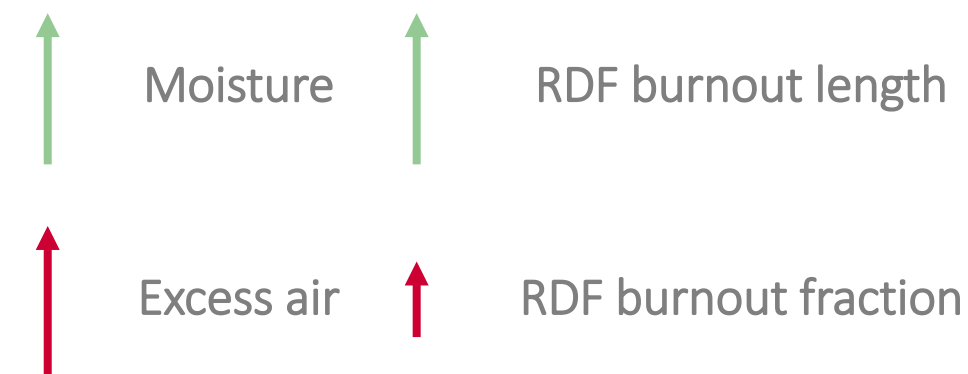
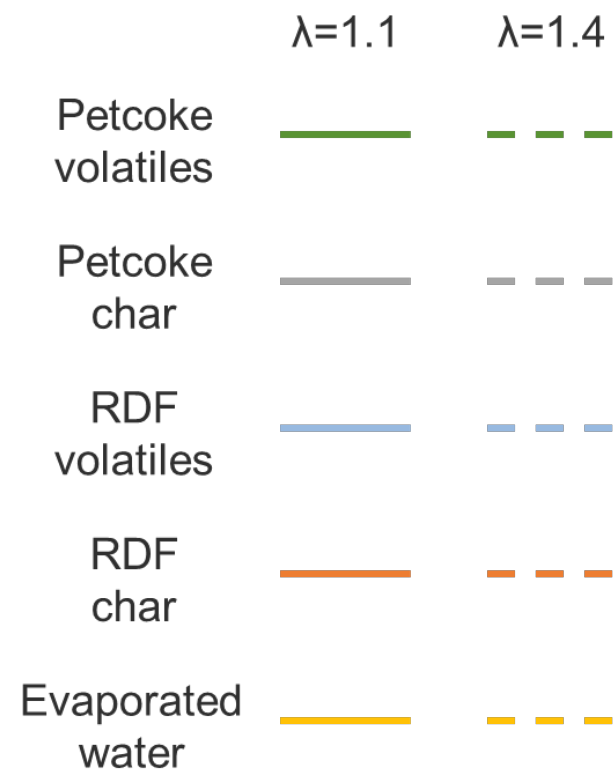
1D model of rotary kiln and cyclone





# 3. Results from validation and fine-tuning

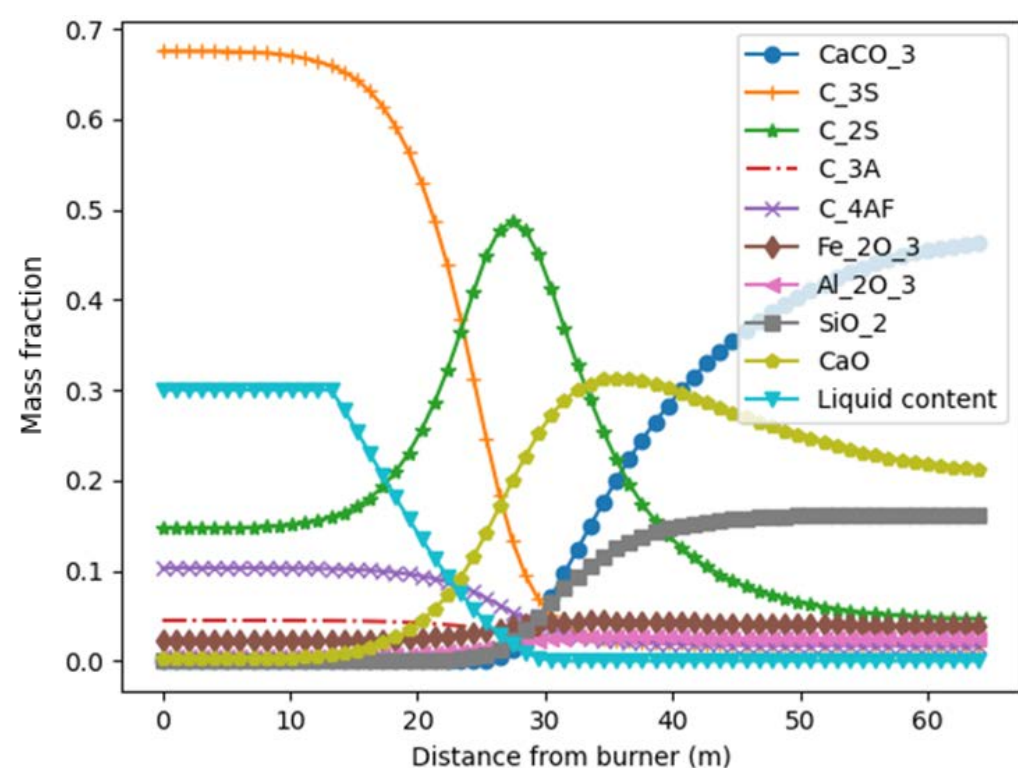
Combustion profiles from CFD simulations



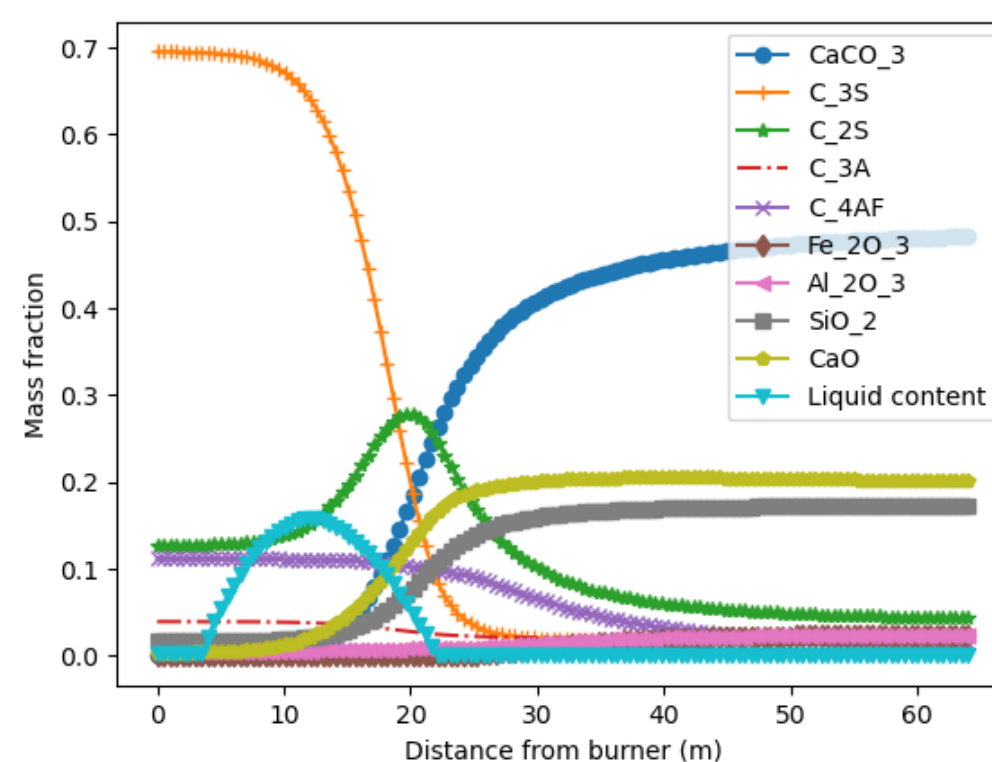
# 3. Results from validation and fine-tuning

A set of 14 empirical parameters exist in the model and were adjusted to match as good as possible 6 validation points, by using metaheuristic methods (Covariance Matrix Adaptation Evolution Strategy).

1<sup>st</sup> DT version



2<sup>nd</sup> DT version



Comparison

- Doubled sampling of kiln slices
- Better melting computation
- More accurate empirical parameters

Species	Mean relative error (%)		
	1 <sup>st</sup> version	2 <sup>nd</sup> version	Diff.
CaCO <sub>3</sub>	0	0.00	0
CaO	78.46	81.38	-2.92
SiO <sub>2</sub>	0.00	0.00	0
C <sub>4</sub> AF	6.14	2.62	3.52
C <sub>2</sub> S	36.58	20.74	15.84
C <sub>3</sub> S	5.57	2.25	3.32
C <sub>3</sub> A	8.82	5.70	3.12
Overall weighted error	10.12	5.35	4.77



# 4. Conclusions

- All fuels have been characterised using historical data and taking into account their variability in time and performing size distribution measurements
- RDF is a very heterogeneous mixture of fuels which needs to be simplified to be introduced in numerical models
- CFD model captures the complex behaviour of RDF particles flight and burning, thus providing useful and accurate information to 1D model, thus accomplishing the task 6.1 objective of proper modelling of alternative fuels. Furthermore, it has been seen that the general flight and burning trajectories of the different RDF modelled is similar, which helps to reduce uncertainties when changing RDF supply
- The modelling approach considered here, a hybrid CFD-1D model, seems to be enough to provide realistic outputs estimation avoiding high computation times for the Decision Support System (DSS)

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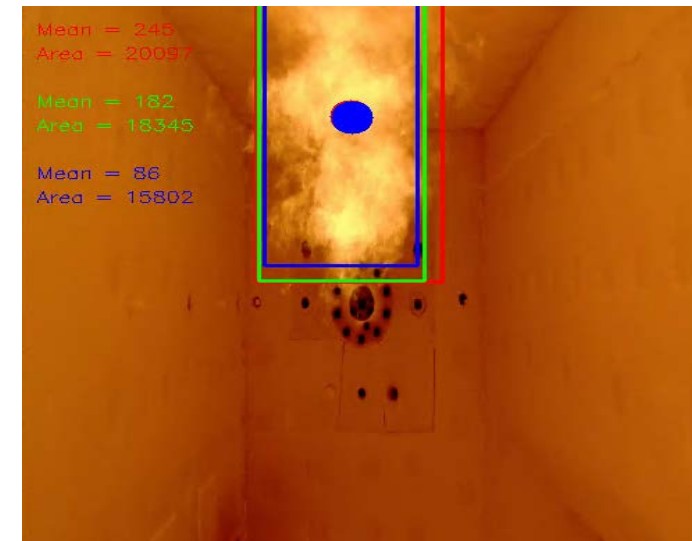
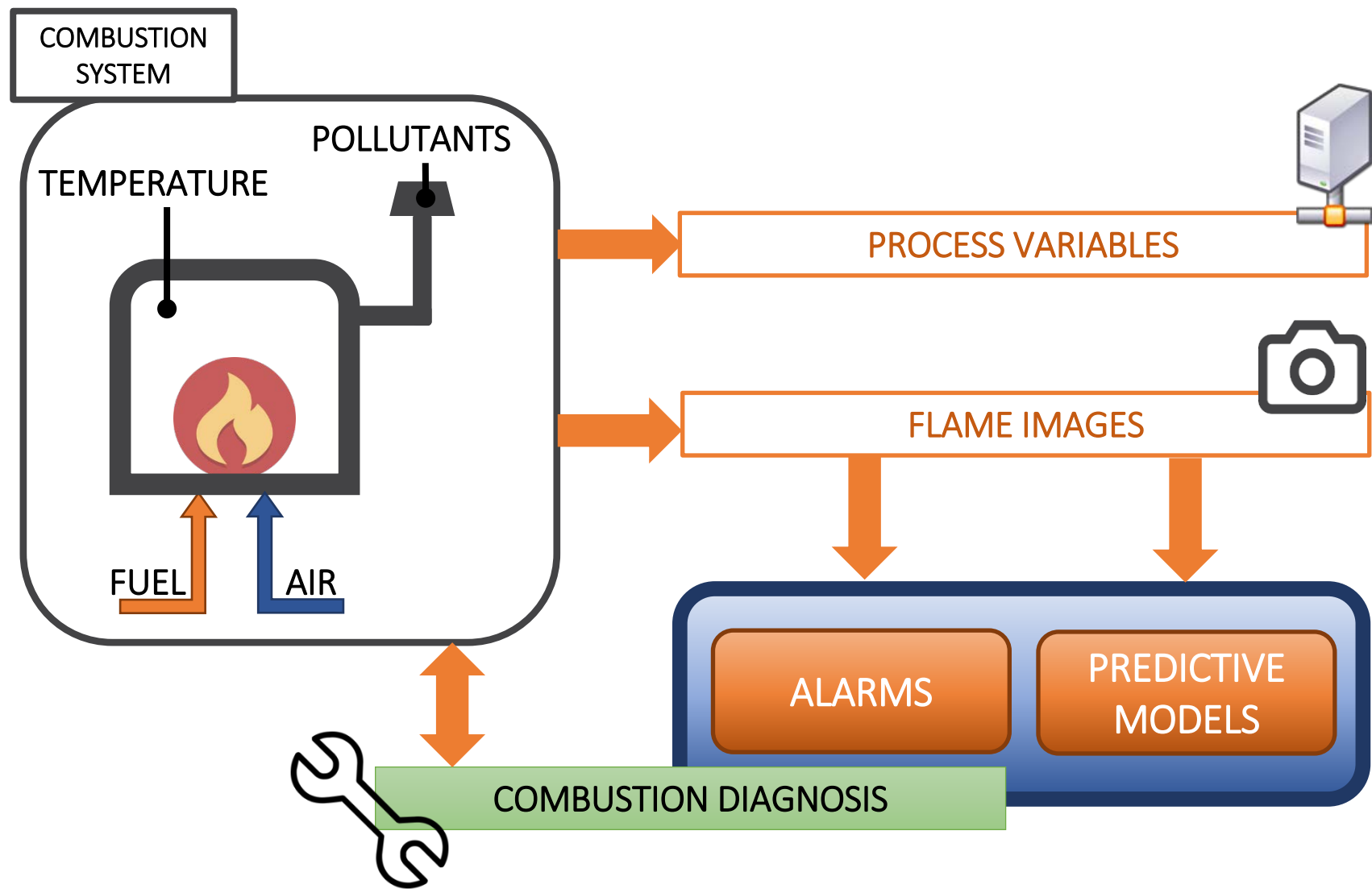
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**FLAME VISUALIZATION  
MONITORING TOOL**  
Jorge Arroyo (CIRCE)

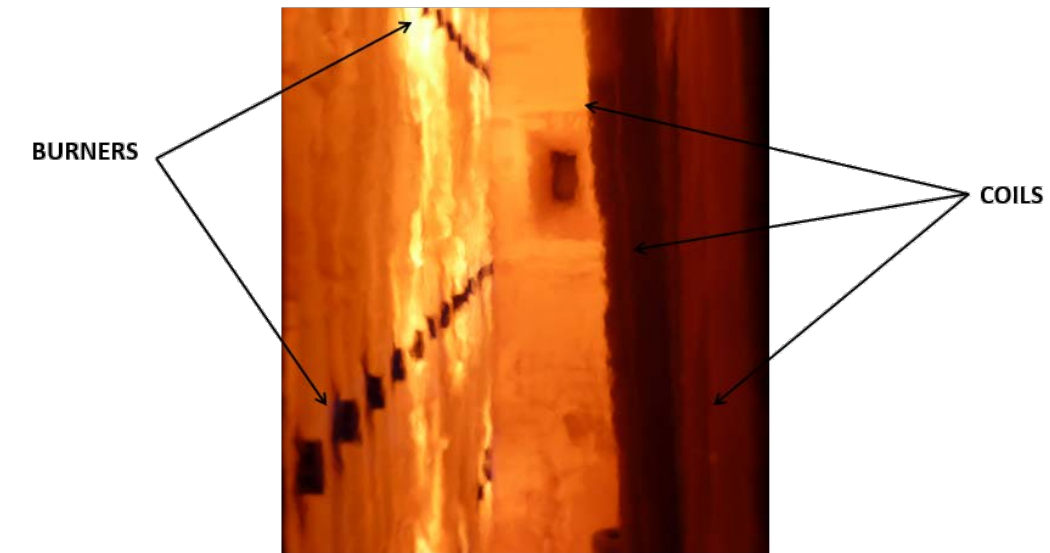
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# Combustion monitoring in RElls



**Steel Sector**



**Chemical Sector**

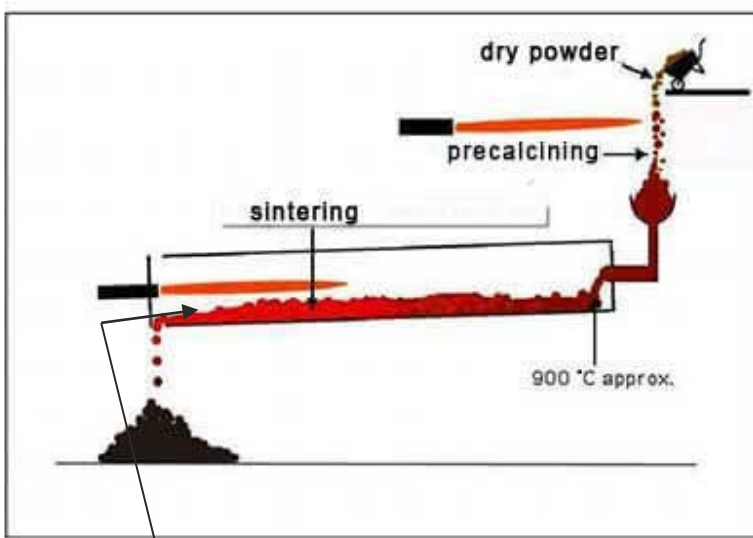


**Laboratory Setup**

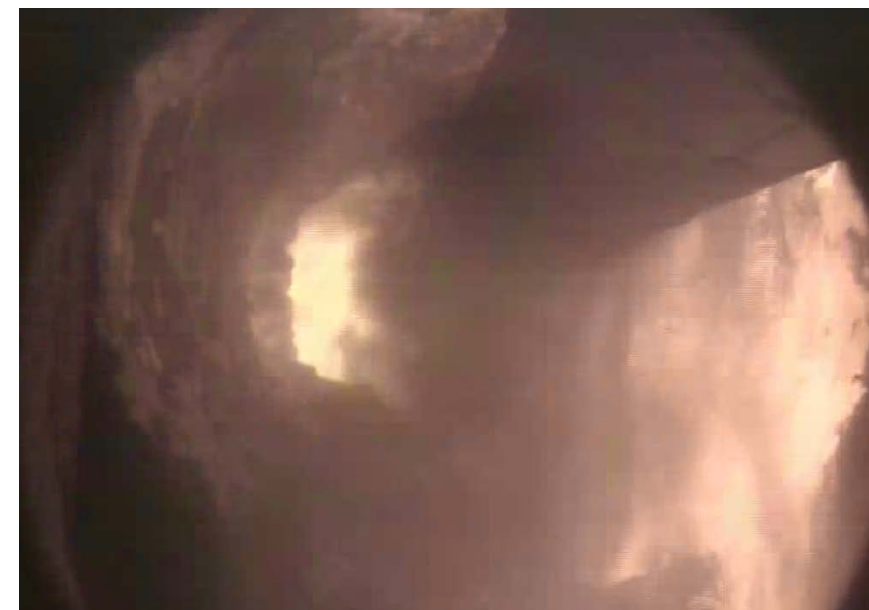
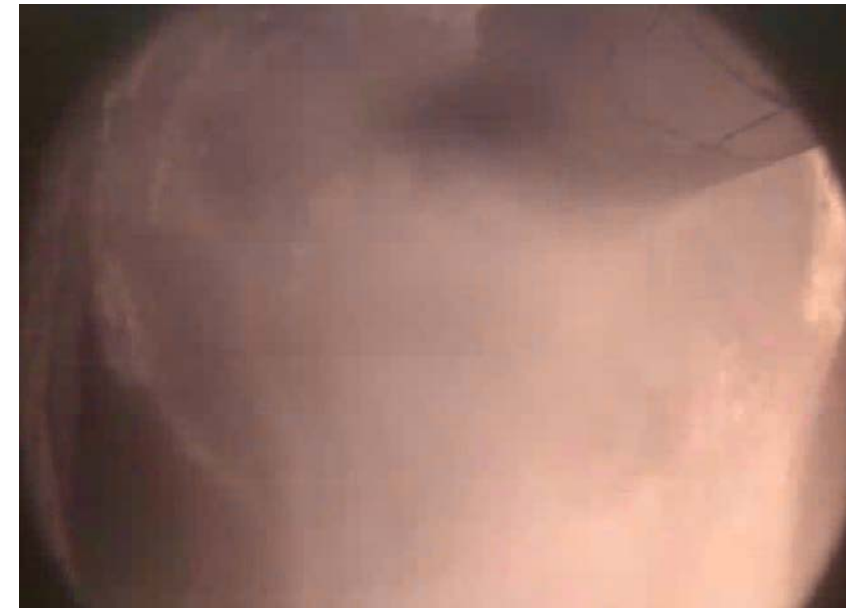
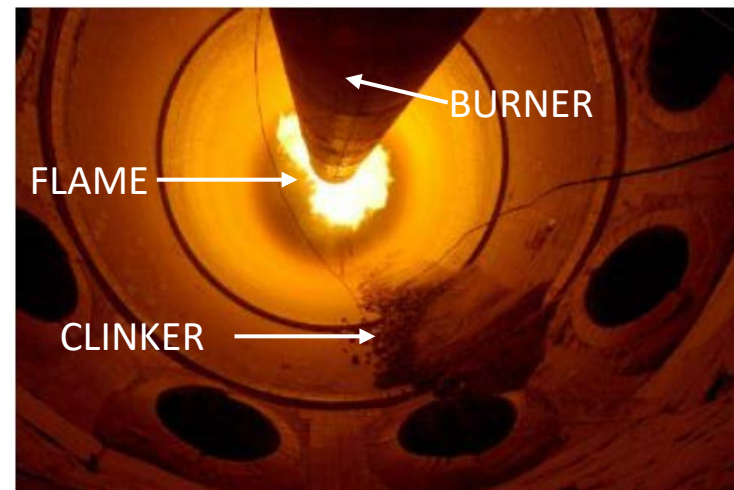




# Combustion monitoring in rotary kilns – RETROFEED



CAMERA

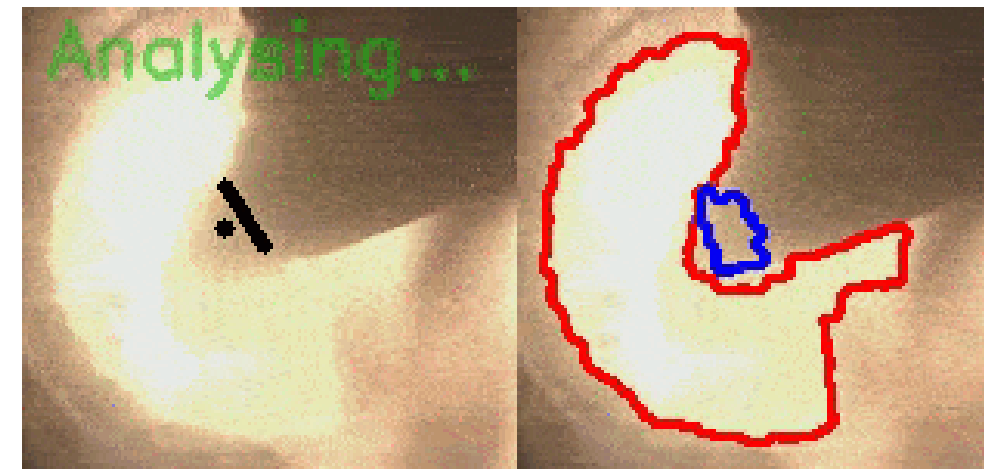
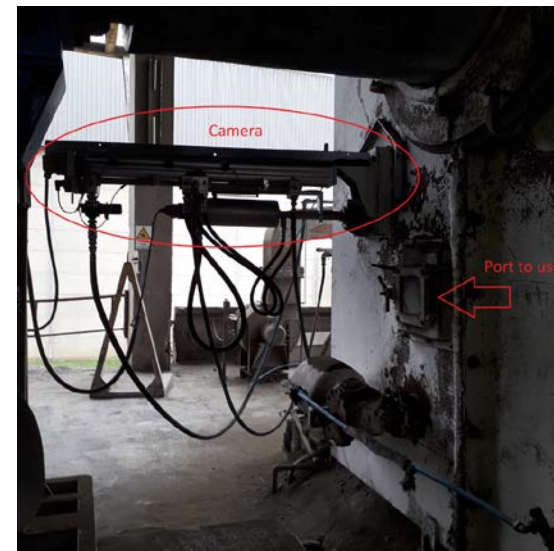
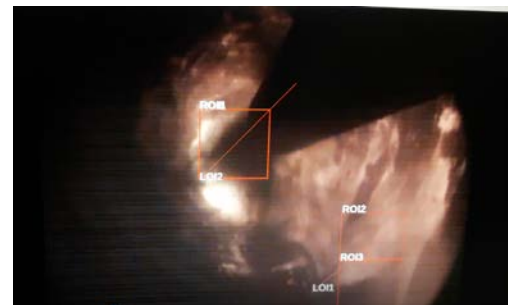


REAL KILN IMAGES



# SECIL rotary kiln case

## USE OF CURRENT ANALOG VIDEO SYSTEM?



### DURAG D-FS 50 FURNACE CAMERA

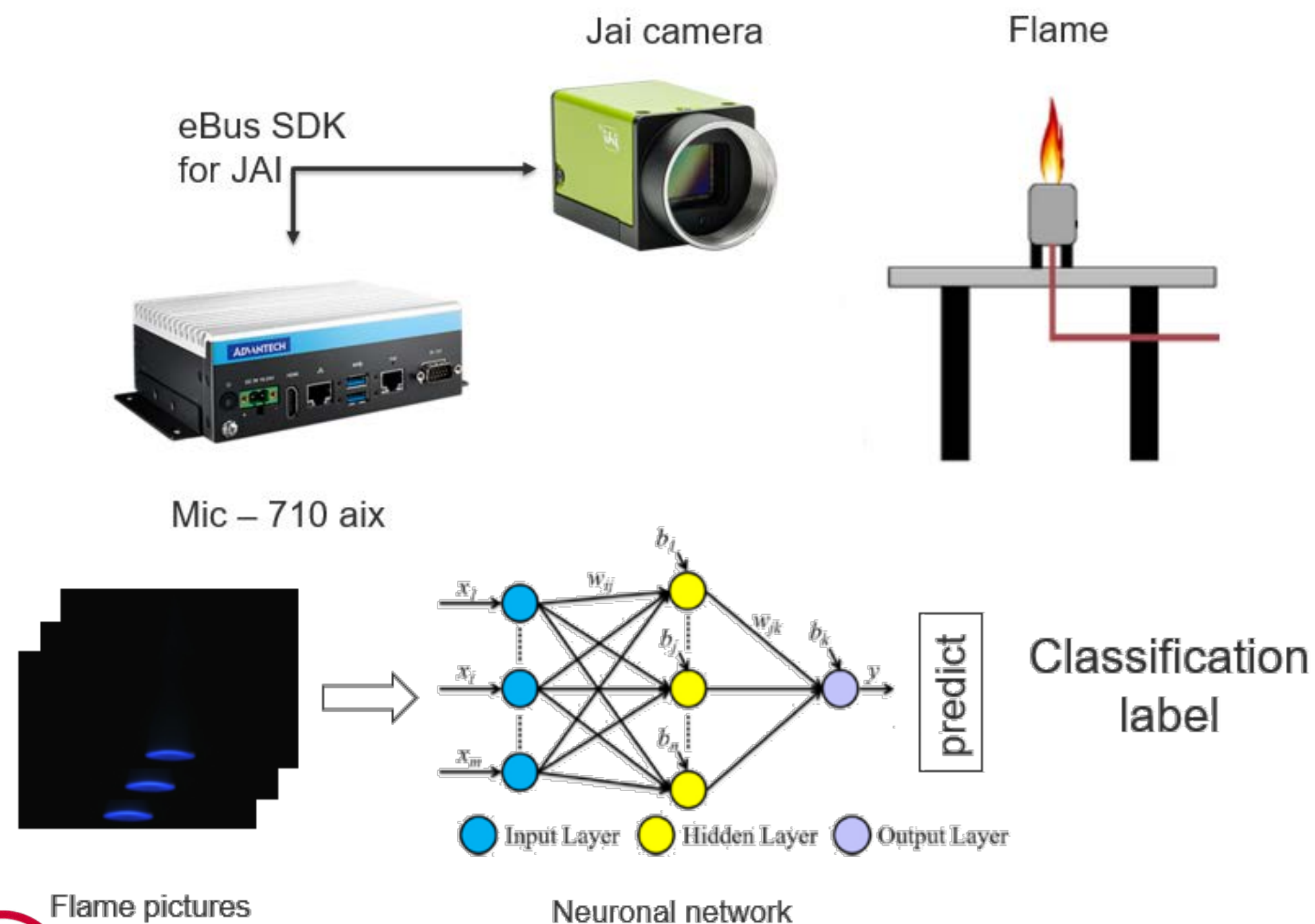
- ✓ No additional installation needed
- ✓ Low investment needed
- ✓ Easier replication in other kilns with camera systems
- ✓ Current camera has the best location
- ✗ Video conversion difficult
- ✗ Camera parameters fixed

- ✓ Video processing feasible with the current system
- ✗ Low quality video
- ✗ Developing algorithms will require a lot of videos and the modification of the parameters

USE OF DURAG  
VIDEO SYSTEM  
OK

# Data acquisition and video processing

## LABORATORY TRIALS -> TEST IA ALGORITHMS UNDER CONTROLLED CONDITIONS



### OBJECTIVE

Acquisition system development for real-time

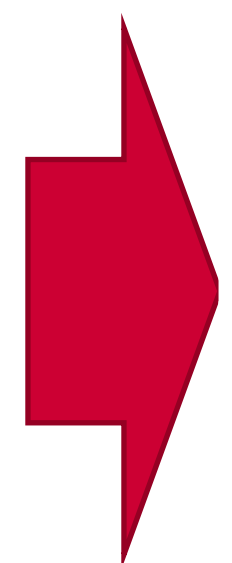
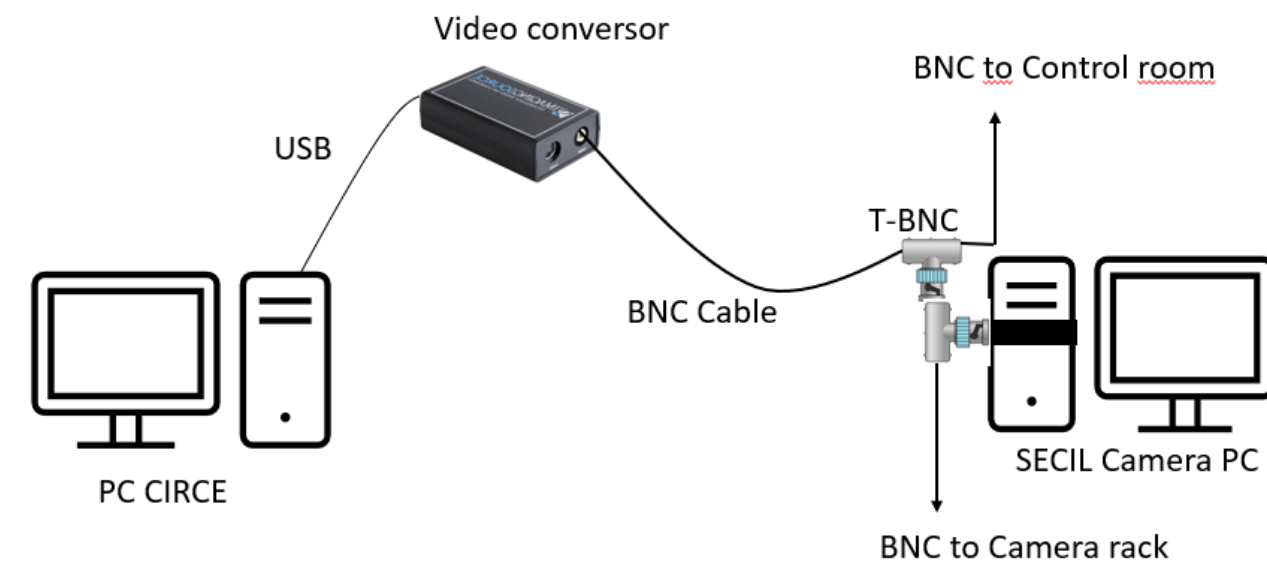
### OBJECTIVE

- Labeling of pictures
- Training neuronal network
- Testing / Validation



# Data acquisition and video processing

INDUSTRIAL TRIALS -> OBTAIN REAL SAMPLES UNDER MULTIPLE WORKING CONDITIONS



Date	Video 1	Video 2	Video 3	Video 4
21/02/2022	8:02:44	8:26:49	8:33:52	9:03:15
22/02/2022	8:21:39	17:45:26	17:54:55	18:01:23
23/02/2022	7:47:16	7:55:12	12:51:57	18:13:44
24/02/2022	13:42:32	15:16:39	17:47:57	
25/02/2022	7:49:21	12:11:00	16:59:18	17:16:08
26/02/2022				
27/02/2022				
28/02/2022	7:53:22	14:45:54	17:46:04	17:52:25
01/03/2022	7:54:56	13:26:53	18:03:47	
02/03/2022	8:02:26	12:09:04	17:26:32	17:32:15
03/03/2022	7:51:39	9:52:38	17:19:58	
04/03/2022	12:26:45			
05/03/2022				
06/03/2022				
07/03/2022				
08/03/2022	8:08:20	13:46:12		
09/03/2022	8:01:45	12:30:52	17:30:49	
10/03/2022	8:00:53	9:33:23	17:01:13	17:14:17
11/03/2022	8:00:57	12:59:30		
12/03/2022				
13/03/2022				
14/03/2022	8:02:41	12:07:33	17:07:29	17:45:23
15/03/2022	8:01:20	12:25:58	17:20:42	
16/03/2022	13:00:56	17:52:46		
17/03/2022	8:06:30	12:02:54		
18/03/2022	8:49:46	12:17:45	13:05:30	
19/03/2022				
20/03/2022				
21/03/2022	8:02:42	13:14:18	17:22:29	
22/03/2022	7:47:07	17:37:26		
23/03/2022	8:01:35	12:15:13	17:21:04	17:41:16
24/03/2022	8:02:47			
25/03/2022	11:47:51	12:52:54		
26/03/2022				
27/03/2022				
28/03/2022	8:28:21	10:57:20	17:45:20	
29/03/2022	8:00:50	18:06:41		
30/03/2022	8:06:23	12:29:42		
31/03/2022	8:36:47	12:42:01		
01/04/2022	13:41:16			
02/04/2022				
03/04/2022				
04/04/2022	15:55:58	17:01:20	17:19:15	

FO6FT_6087	Raw Meal Flow to Kiln	t/h	
AR6LCC_F	LCC Feed	t/h	
FO6SIC_6101	Kiln Speed	rpm	
FO6II_6101_FILT	Kiln Current	A	
FO6DO6141_F	Coal Feeder Flow	t/h	
FO6PCA414_F	Alternative Fuels Flow	t/h	
FO6DO6500_F	Tyre Feed Rate	t/h	
FO6DOH2_Running	Hydrogen Feed		
FO6DOH2_2_F	Hydrogen Unit 2 Flow	%	
SMQFO6Energy01Pct1	Energy Desired Setpoint	%	Coal
SMQFO6Energy04Pct1	Energy Desired Setpoint	%	RDF
SMQFO6Energy06Pct1	Energy Desired Setpoint	%	Tyres
SMQFO6Fuel01PCI	Burning Value with water	kcal/kg	Coal
SMQFO6Fuel04PCI	Burning Value with water	kcal/kg	RDF
SMQFO6Fuel06PCI	Burning Value with water	kcal/kg	Tyres
PCAFUEL08RECIPEPERC	Parque de Combustiveis Alternativos - Fuel #8 Volumetric Recipe Percentage	%	RDF Very High
PCAFUEL10RECIPEPERC	Parque de Combustiveis Alternativos - Fuel #10 Volumetric Recipe Percentage	%	RDF High
PCAFUEL11RECIPEPERC	Parque de Combustiveis Alternativos - Fuel #11 Volumetric Recipe Percentage	%	RDF Medium
PCAFUEL12RECIPEPERC	Parque de Combustiveis Alternativos - Fuel #12 Volumetric Recipe Percentage	%	RDF Low
SMQFO6MainPCI	Mean PCI in main burner	kcal/kg	
SMQFO6EnergySumPct1Main	Sum of Energy Pct to Main Burner	%	
SMQFO6EnergySumPct1Calc	Sum of Energy Pct to Calciner	%	
SMQFO6EnergySumMWMMain	Sum of MW to Main Burner	MW	
SMQFO6EnergySumMWCalc	Sum of MW to Calciner	MW	
SMQFO6EnergySumMWTot	Sum of MW to Kiln Total	MW	
FO6SIC_6142	Primary Air Fan Speed	rpm	
FO6O2_6461	O2 6th Floor	%	
FO6AI_6461	CO 6th Floor	%	
FO6NO_6461	NO 6th Floor	ppm	
FO6SO2_6461	SO2 6th Floor	ppm	
FO6PT_6385	ExhaustFan 6103 Outlet Pressure	mmca	
FO6SIC_6103	Exhaust Fan 6103 Speed	rpm	
FO6IIAH_6103	Exhaust Fan 6103 Power	kW	
FO6PT_6370	ExhaustFan 6103 Inlet Pressure	mmca	
FO6PT_6371A	Cyclone 1A Outlet Pressure	mmca	
FO6PT_6371B	Cyclone 1B Outlet Pressure	mmca	
FO6PT_6372	Cyclone 2 Outlet Pressure	mmca	
FO6PT_6369	Cyclone 3 Outlet Pressure	mmca	
FO6PT_6368	Cyclone 4 Outlet Pressure	mmca	
FO6PT6387	Kiln Outlet Pressure	mmca	
FO6TT_6320	Exhaust Fan Inlet Temperature	°C	
FO6TT_6321A	Cyclone 1A Temperature	°C	

Process Data

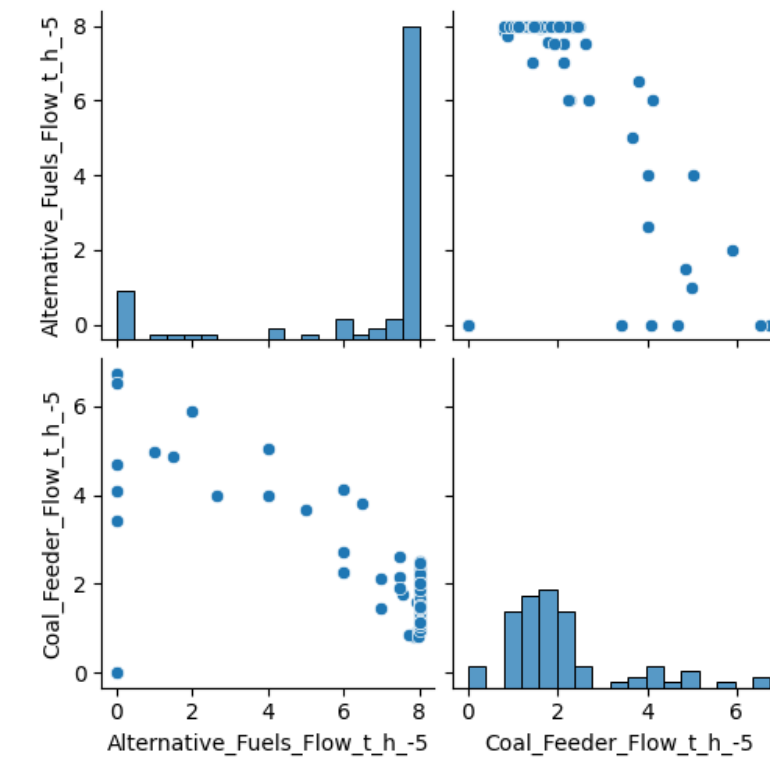
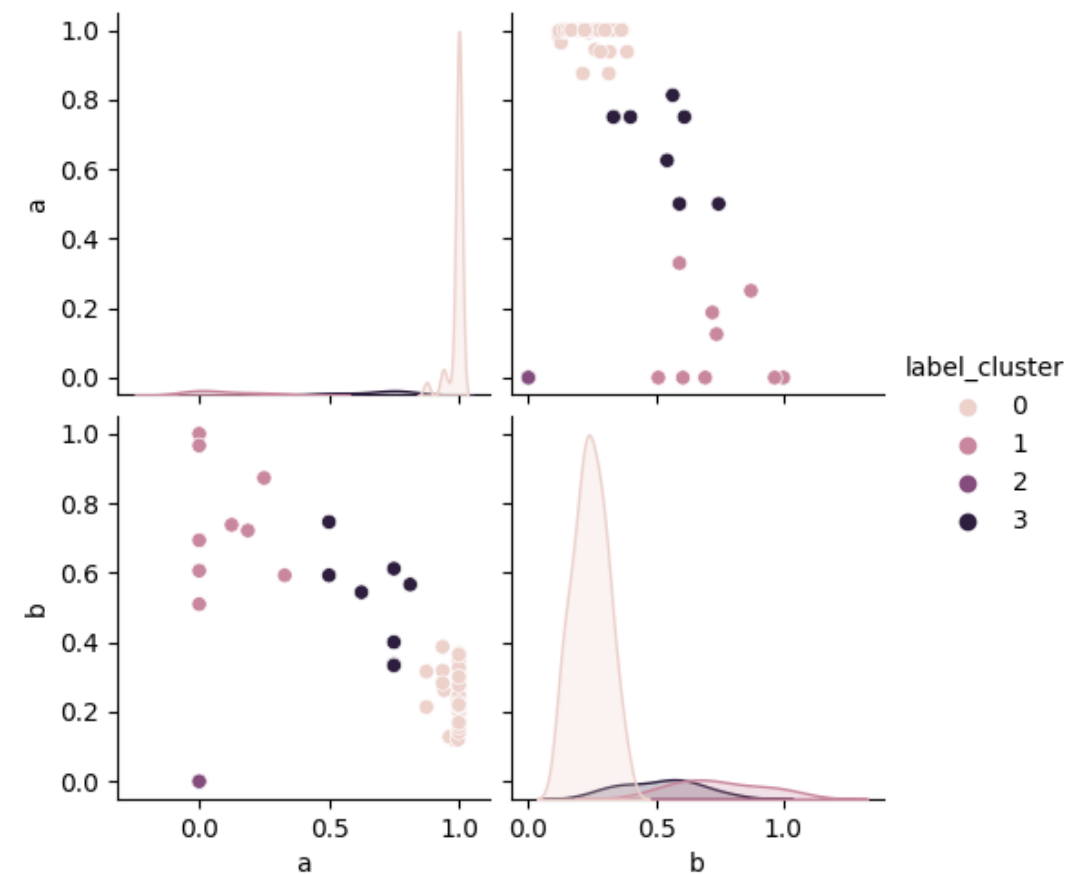
Video Campaign

# Data processing

## CLUSTERING -> SELECT VIDEOS AND CONDITIONS SUITABLES FOR PROCESSING

0			
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-31 12-42-01	8.0	1.525926	80
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-04-01 13-41-16	8.0	2.029459	81
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-04-04 15-55-58	8.0	1.139283	82
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-04-04 17-01-20	8.0	1.139413	83
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-04-04 17-19-15	8.0	1.487507	84
1			
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-02-21 17-03-49	0.0	6.748262	4
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-02-23 18-13-44	0.0	6.52	12
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-01 13-26-53	2.0	5.891965	25
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-11 08-00-57	0.0	3.439849	44
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-18 08-49-46	0.0	4.09	57
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-21 08-02-44	1.5	4.87	60
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-21 17-22-29	1.0	4.981181	62
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-28 08-28-21	0.0	4.68	72
3			
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-02-24 15-16-39	4.0	4.0	14
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-03 09-52-38	4.0	5.036416	32
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-09 12-30-52	2.634906	4.0	38
2			
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-02 17-26-32	0.0	0.0	29
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-02 17-32-15	0.0	0.0	30
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-18 12-17-45	0.0	0.0	58
Alternative_Fuels_Flow_t_h_-5	Coal_Feeder_Flow_t_h_-5	A	
Video_name			
22-03-18 13-05-30	0.0	0.0	59

Clustering using two most relevant variables by k-means



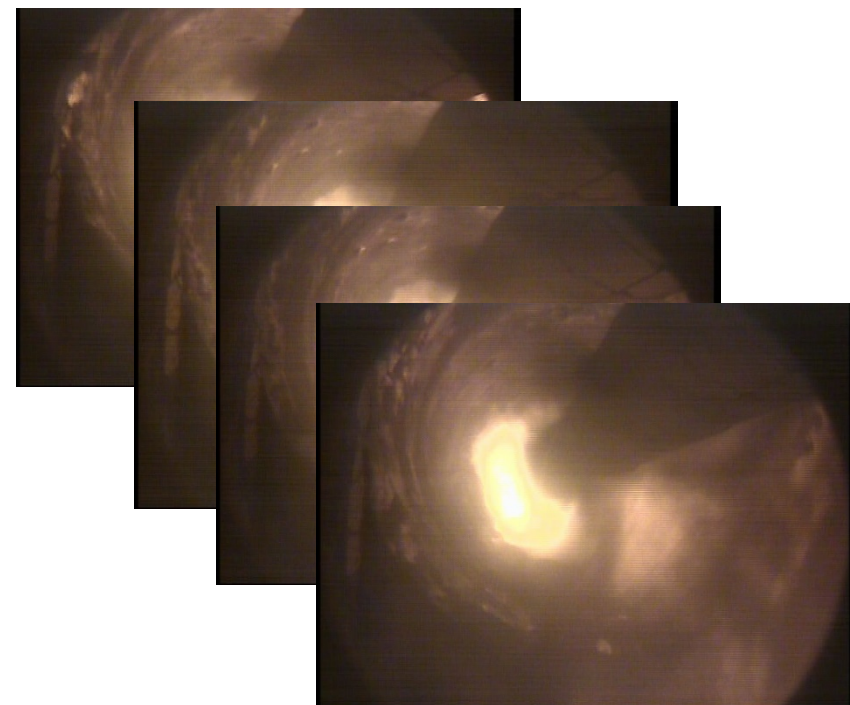
a = Alternative\_Fuels\_Flow\_t\_h\_-5, b = Coal\_Feeder\_Flow\_t\_h\_-5, c = Kiln\_Current\_A+15, d = Kiln\_Speed\_rpm  
 e = Primary\_Air\_Fan\_Speed\_rpm, f = Raw\_Meal\_Flow\_to\_kiln\_t\_h\_+15, g = Secondary\_Air\_Temperature\_Celsius+15'



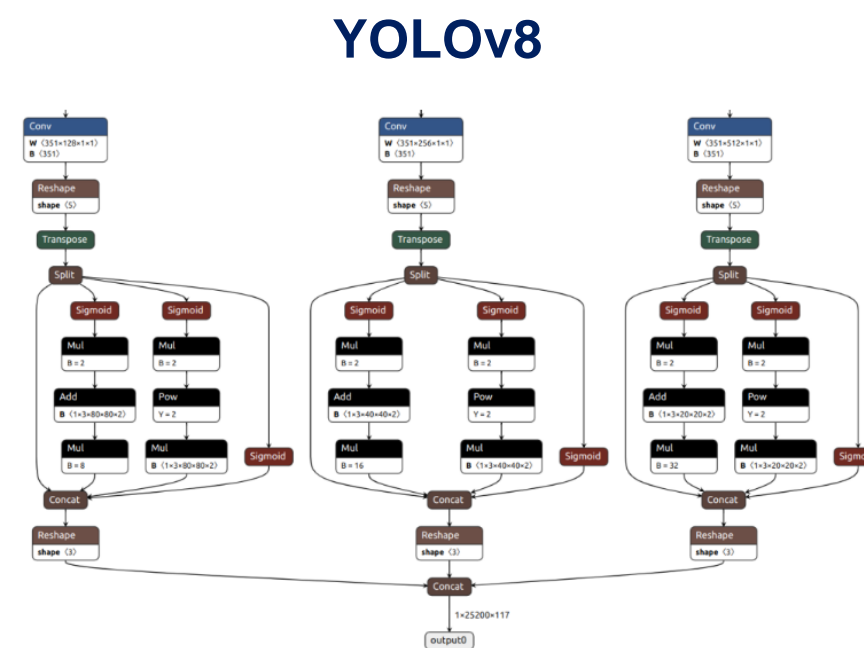
# Flame monitoring development

## TRAINING PROCESS -> USE OF DEEP LEARNING YOLO V8

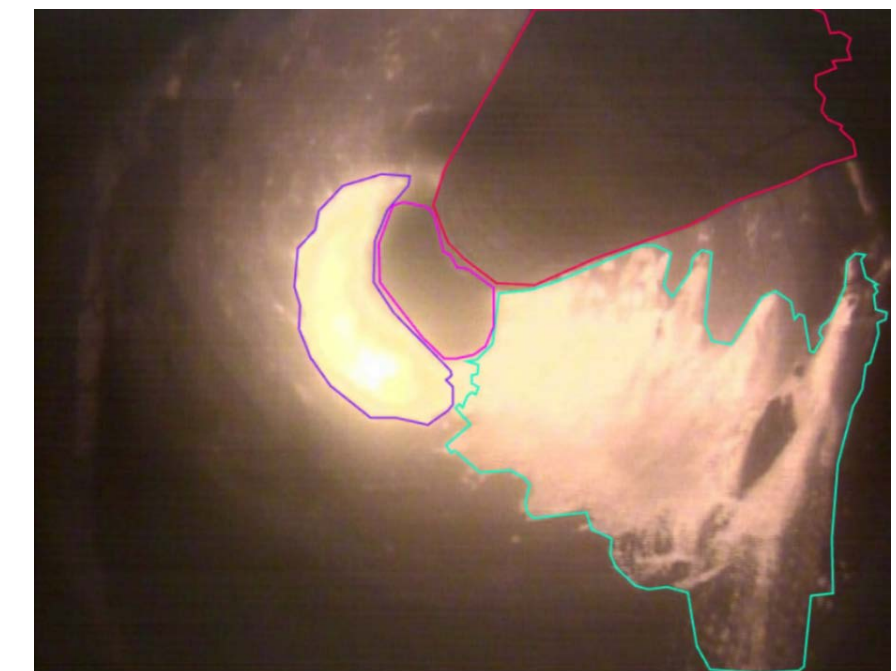
Input



Model for Real Time Instance Segmentation



Output



# Flame monitoring application



- Graphical interface
- Segmentation of elements
- Element identificación
- Area characterization
  - Geometrical features
  - Statistical features
  - Texture features
- Real time updates



# Future developments

- Validation under real conditions (long periods of time) -> Feedback from operators
- Correlation with process variables: On a first step offline, on a second step on real time
- Replication in other plants and in other sectors

# TOWARDS MORE EFFICIENT CEMENT INDUSTRIES

ONLINE TECHNICAL WORKSHOP

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**QUALITY MEASUREMENT  
MONITORING SYSTEM FOR CLINKER**  
Francisco Rodriguez (AIMEN)



This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 869939.

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# Objectives and challenges

## **Objectives:**

- Measure **temperature and clinker size** at SECIL cement factory
- **Estimate CCN phase** (freelime, C2S, C3S...)

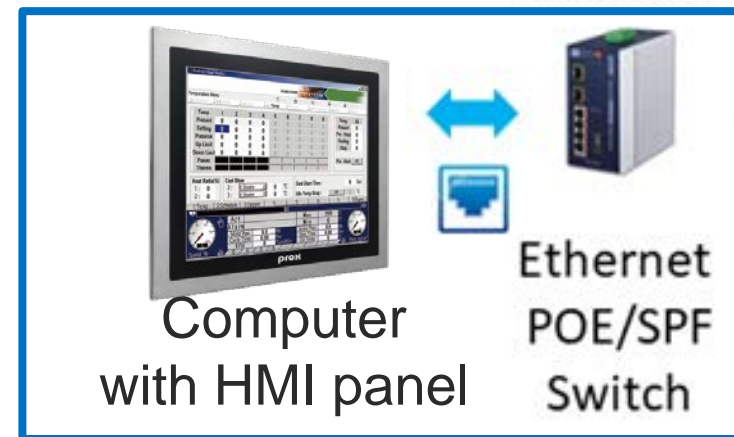
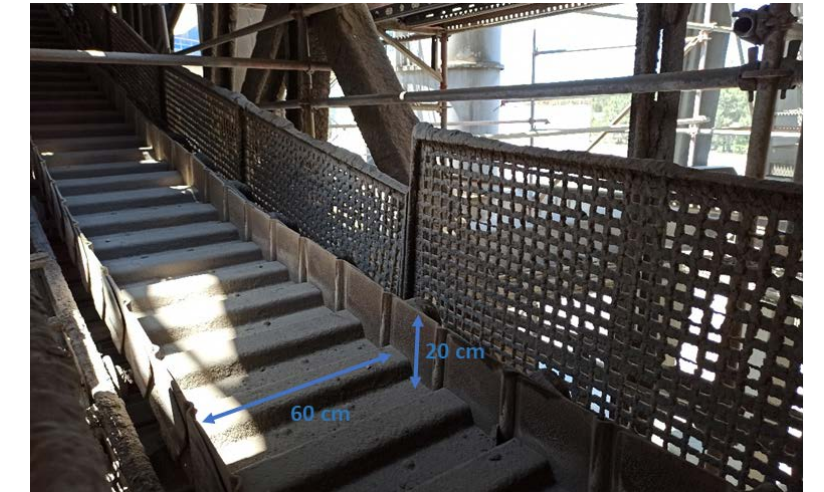
## **Challenges:**

- **Harsh environment** : sensors selection (robustness and accuracy), devices protection
- **Factory integration**: Modular systems, How to simulate factory environment for optimize development and validation? How to integrate without stopping or reducing production?
- **System architecture**: data transmission (long distances), data flow management
- **Data analysis**: processing strategies, results

# General architecture for monitoring system deployed in factory



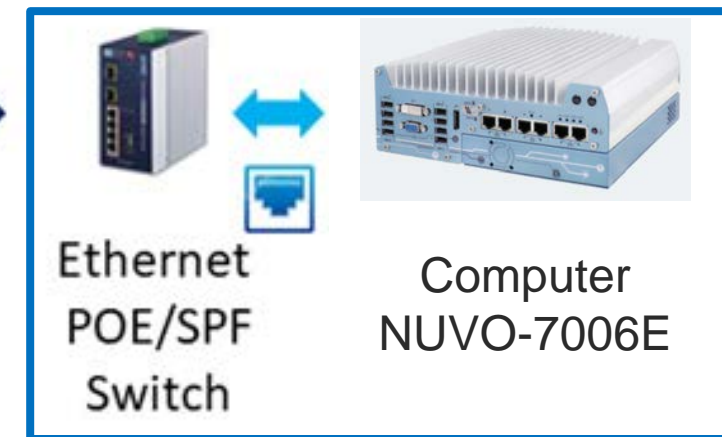
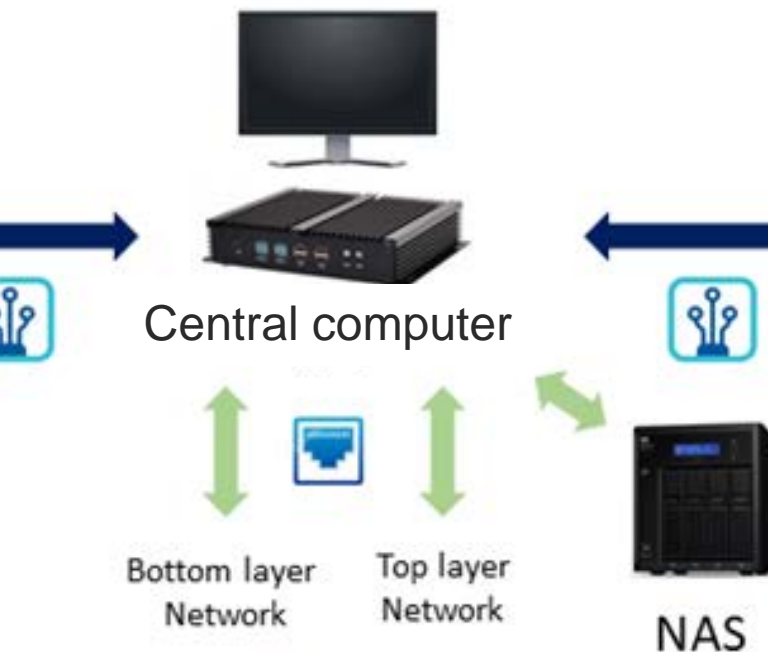
Online monitoring system



Electrical cabinet



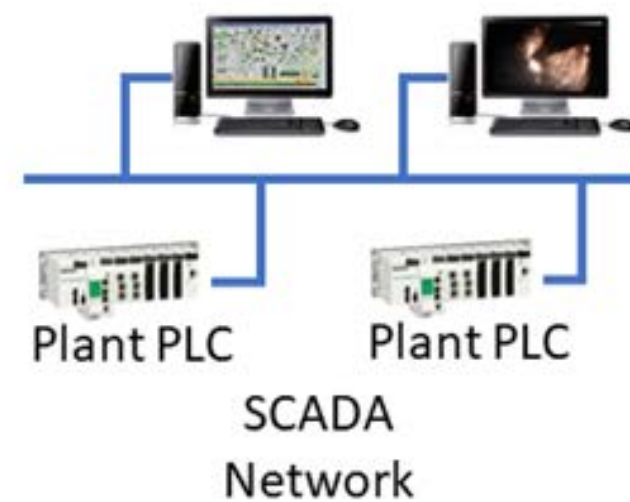
Phase estimation (C3S, C2S, Frelime...)  
Size and temperature of clinker samples



Electrical cabinet



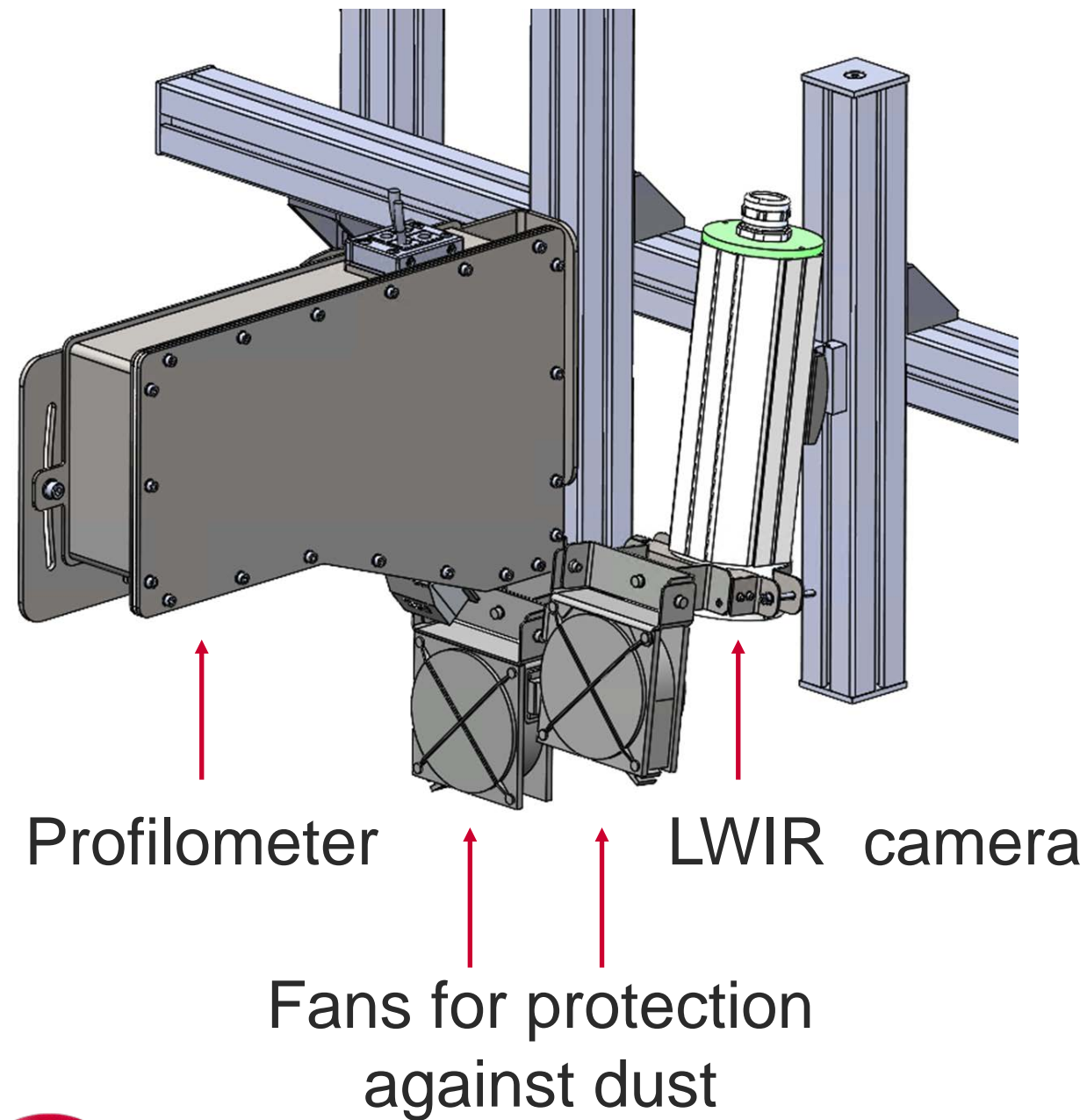
Size and temperature of clinker flow



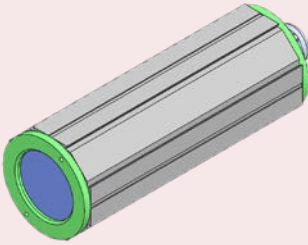
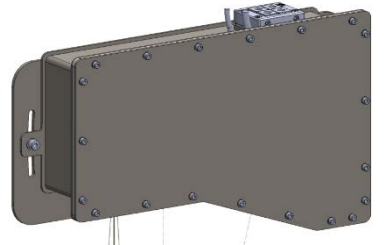


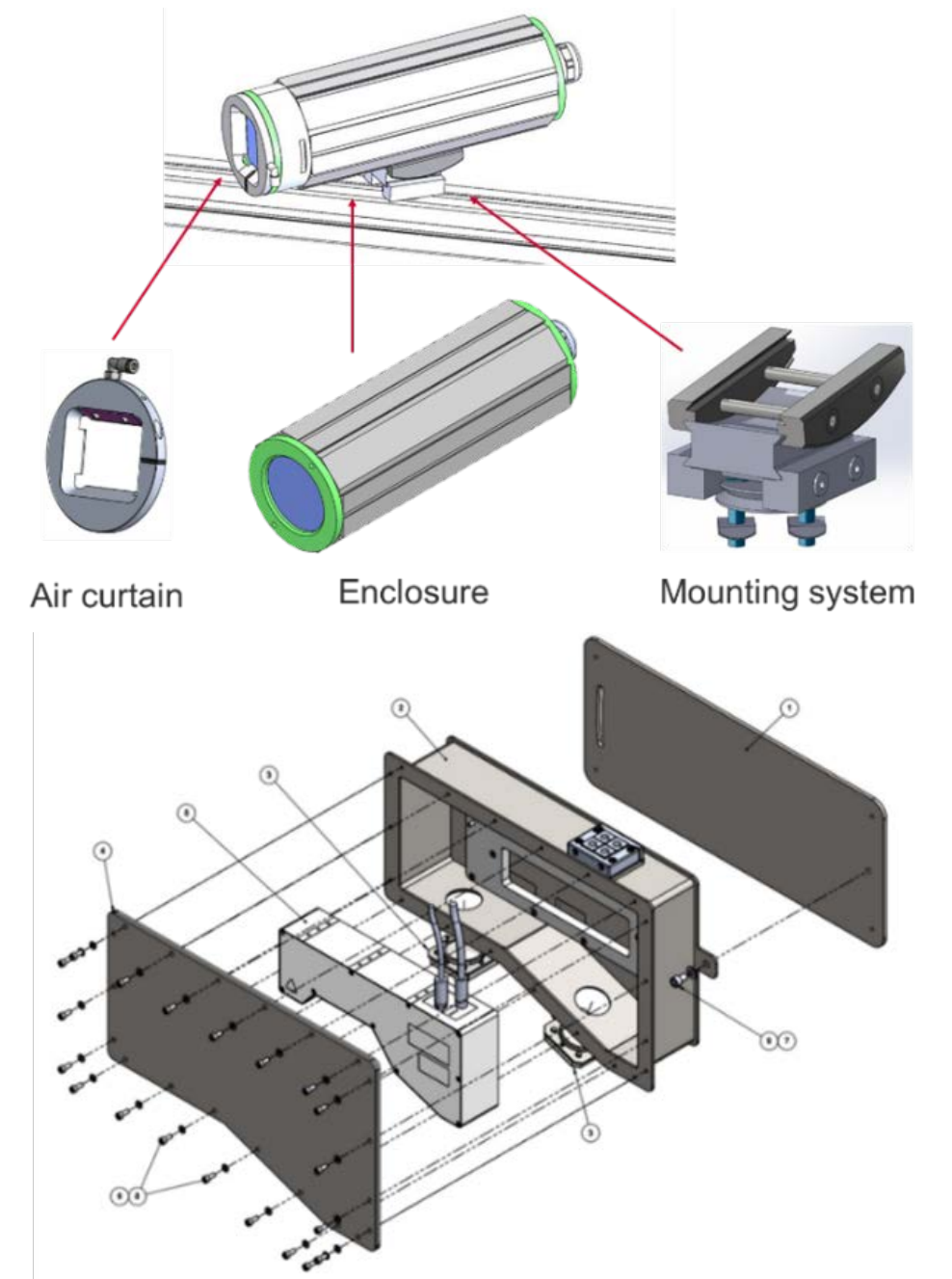


# Temperature and size for transportation belt : mechanical system

## Clamping and protection system



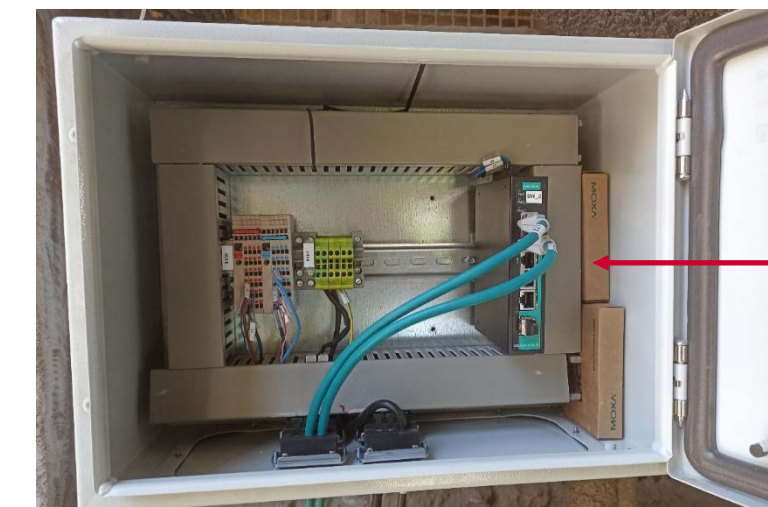
CAMERA	PROFILOMETER
	
IRSX 640 Compact	Compact Sen. C5-2040CS19-640
AT (Automation Technology)	AT (Automation Technology)
	
ORCA camera enclosure (IP67)	Designed for profilometer (IP65)
Autovimination	AIMEN



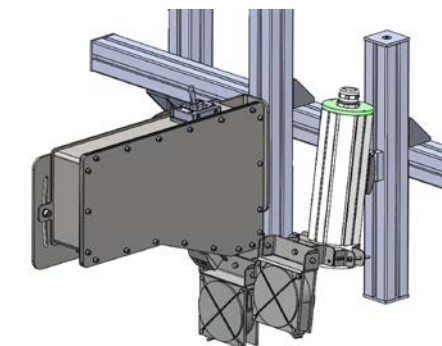
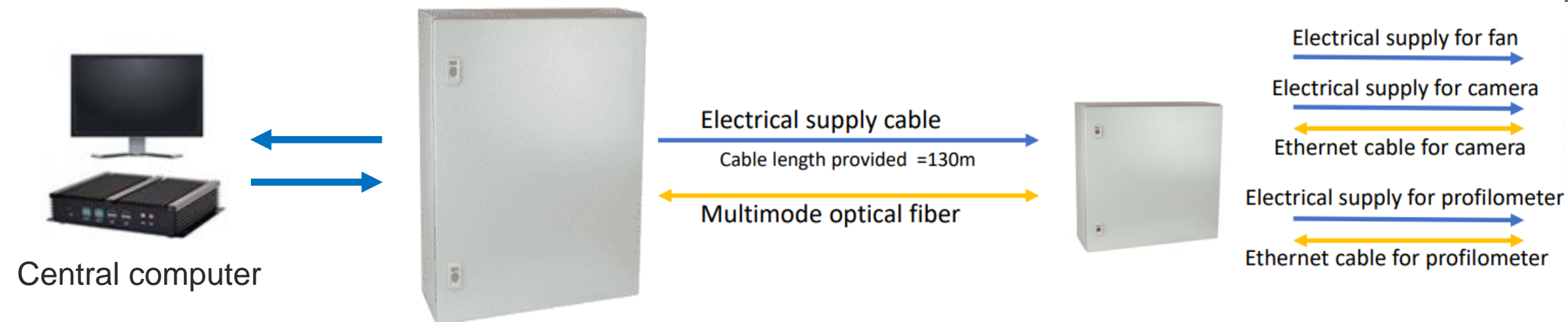
Windows with air curtains are mounted on both systems for ensuring protection against dust



# System integrated in transportation belt in SECIL factory

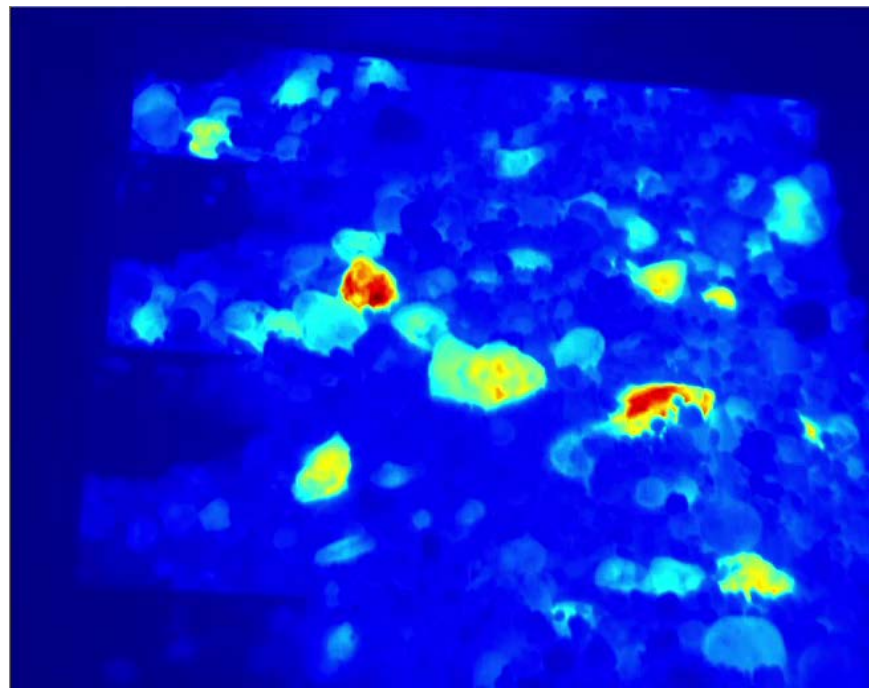


Com system  
Optical fiber  
router

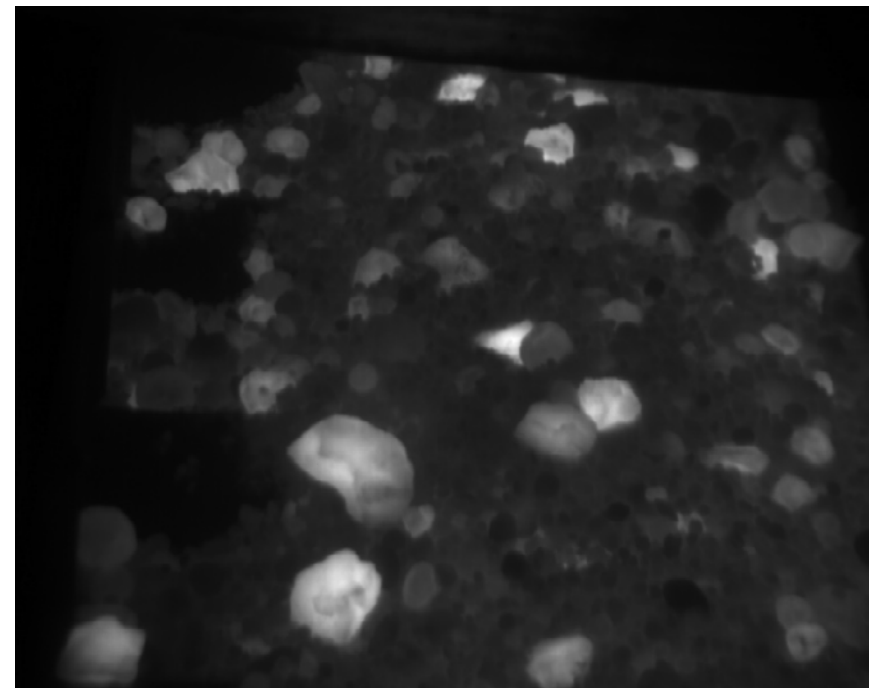




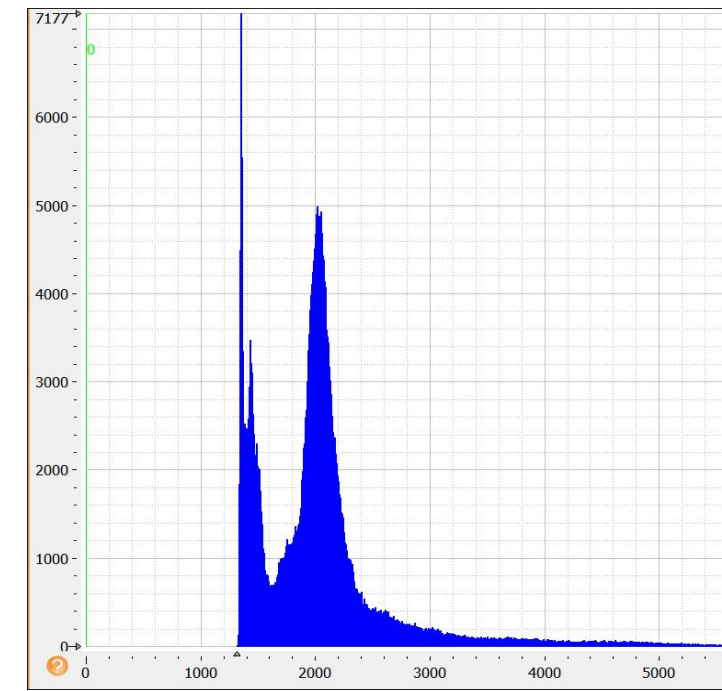
# Temperature and size: results from acquisition on transportation belt



Thermal video



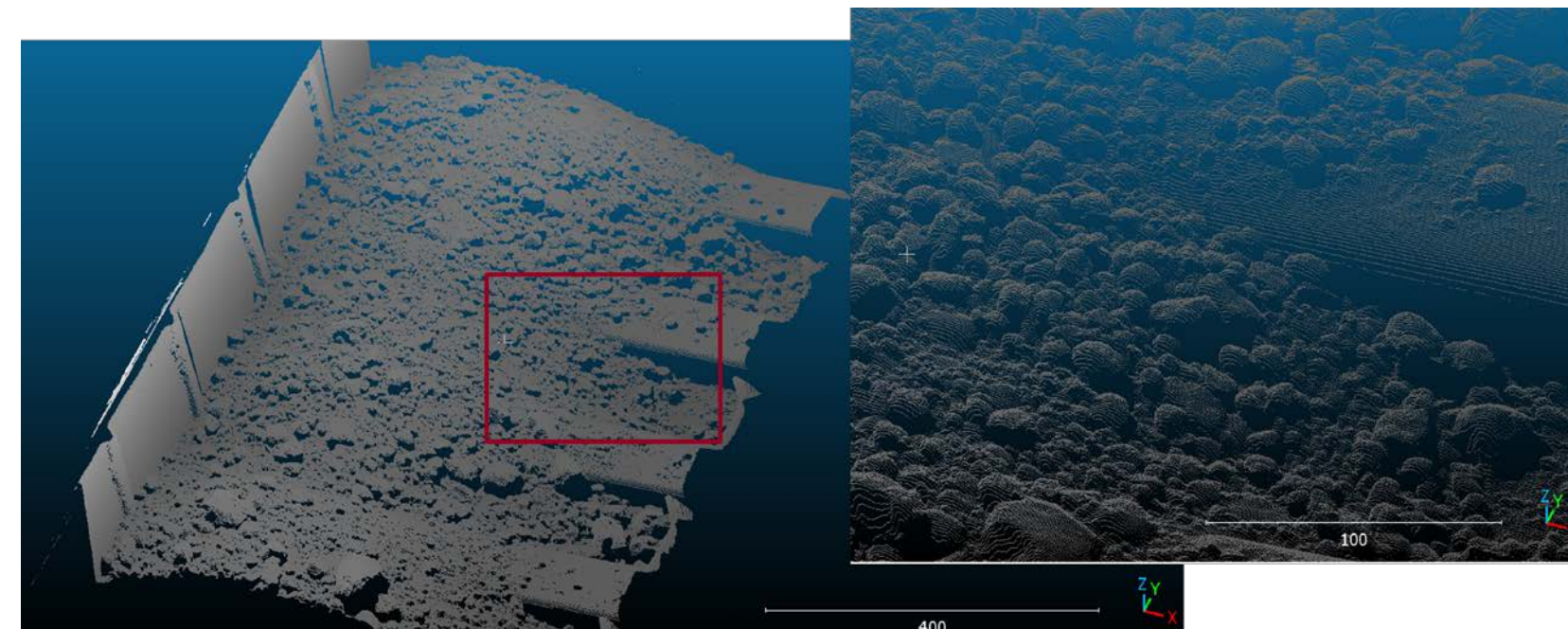
Thermal gray scale image



Temperature Histogram distribution



Laser line projected on clinkers flow

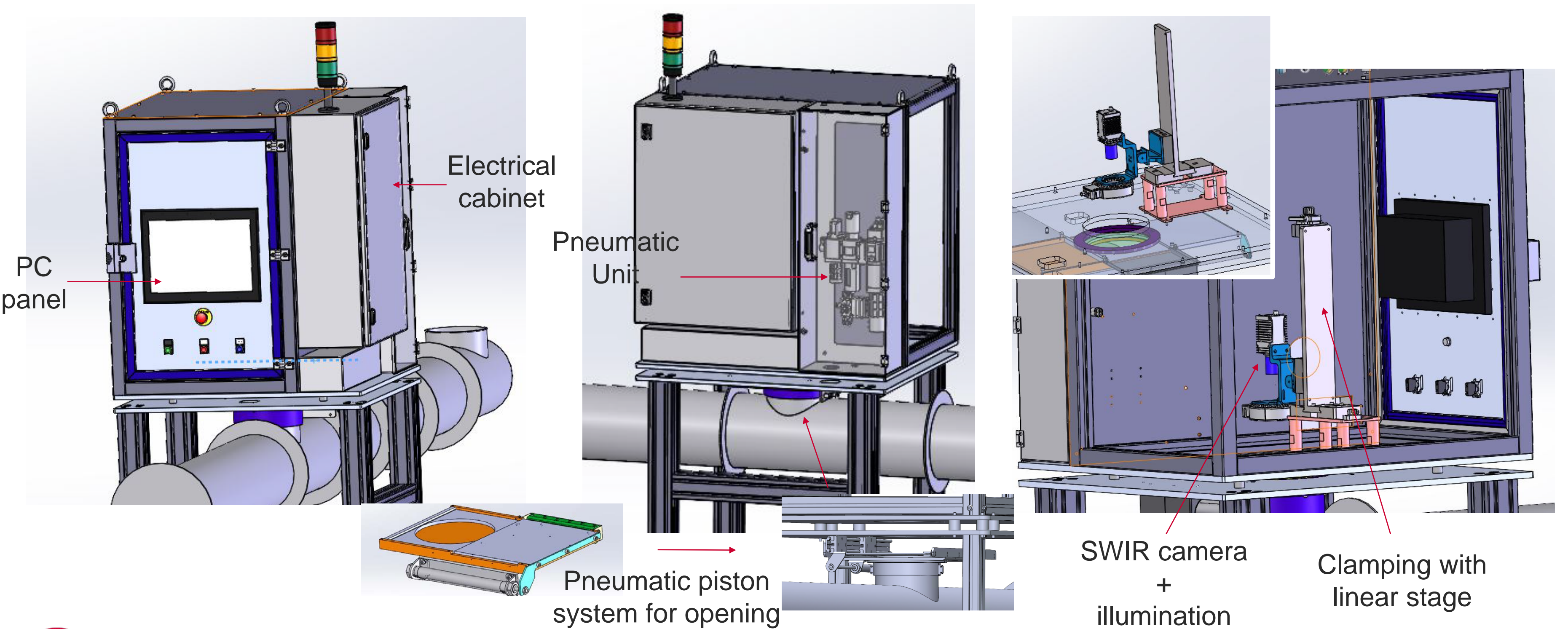


Point cloud obtained from profilometer





# Temperature and size measurement: enclosure system for conveyor pipe



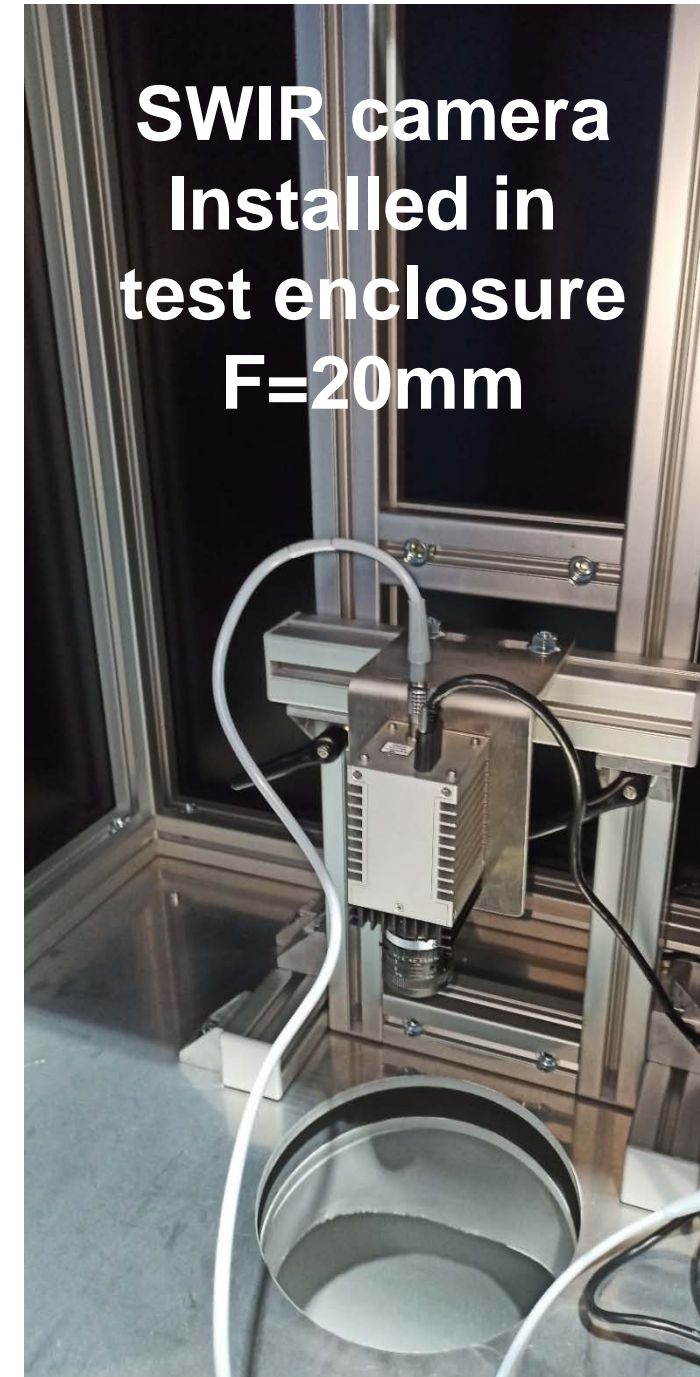
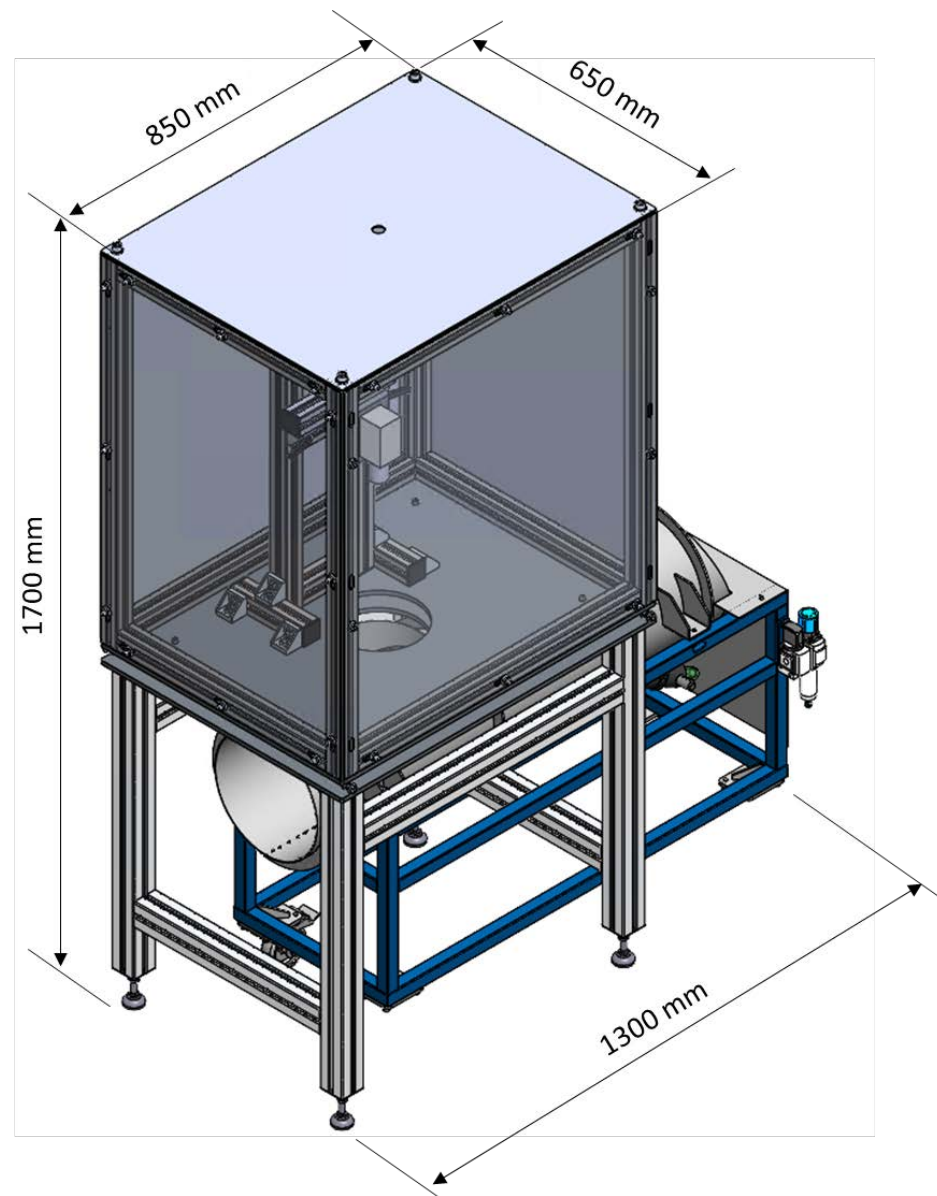


# Enclosure system assembly and test at AIMEN facilities





# Testing bench developed at AIMEN for simulating clinker on pipe



Conveyor pipe system

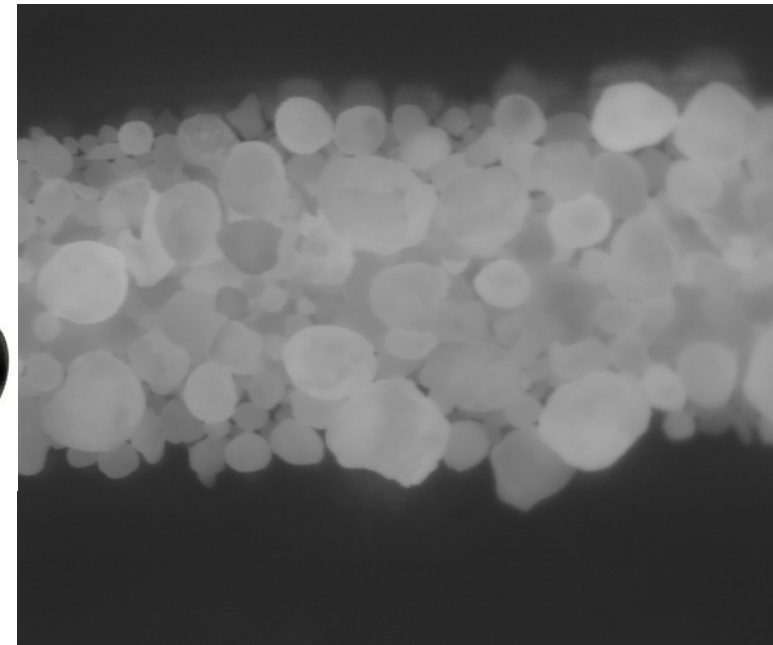


Clinker flow simulated

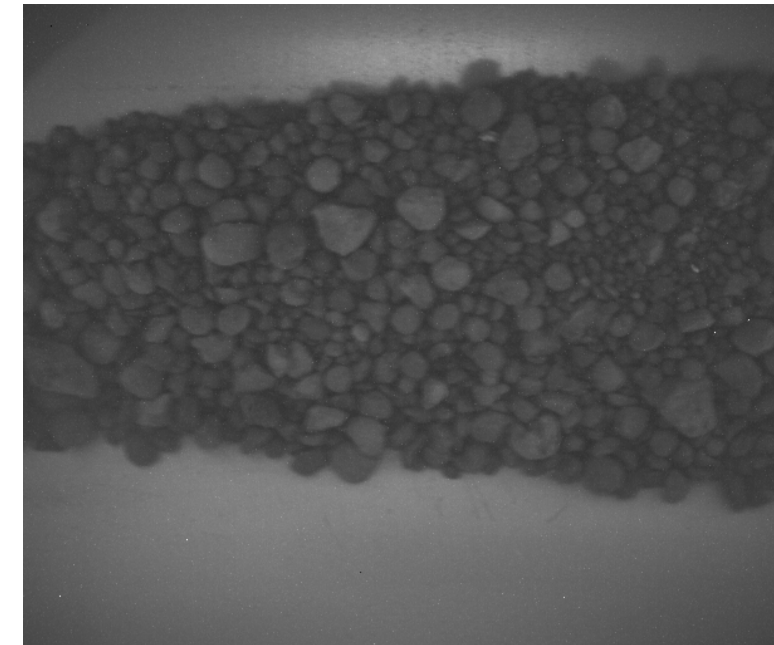


# Infrared and size measurements on conveyor pipe

EO spec.	Gobi GigE Xenics
Image format	640x480 pxs
Pixels pitch	17 $\mu\text{m}$
Detector type	a-Si microbolometer
Active area	10,88 x 8,16 mm
Spectral range	[8-14] m
Max. FP full	60 Hz
Digital output	GigE



LWIR image

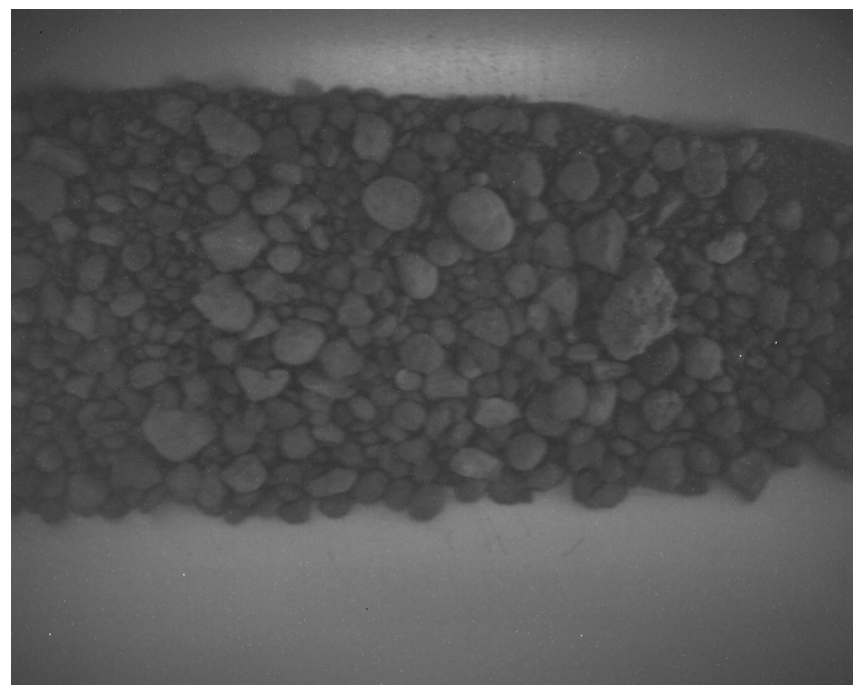


SWIR image



EO spec.	Wildcat UV3100 Xenics
Image format	640x512 pxs
Pixels pitch	20 $\mu\text{m}$
Detector type	InGaAs
Active area	12,8x10,24 mm
Spectral range	[900-1700] nm
Max. FP full	110 Hz
Digital output	USB3 Vision

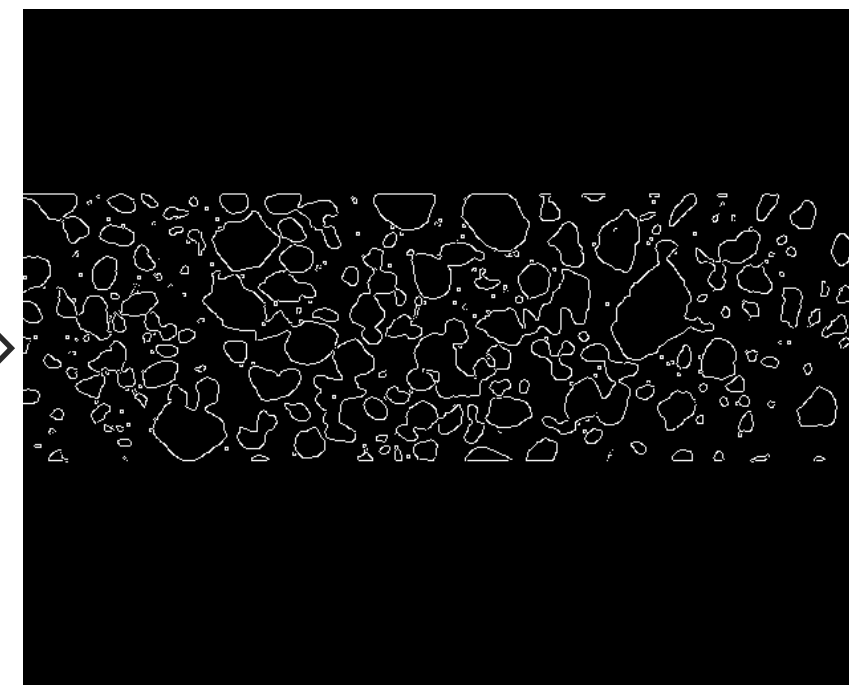
## Segmentation example for size estimation:



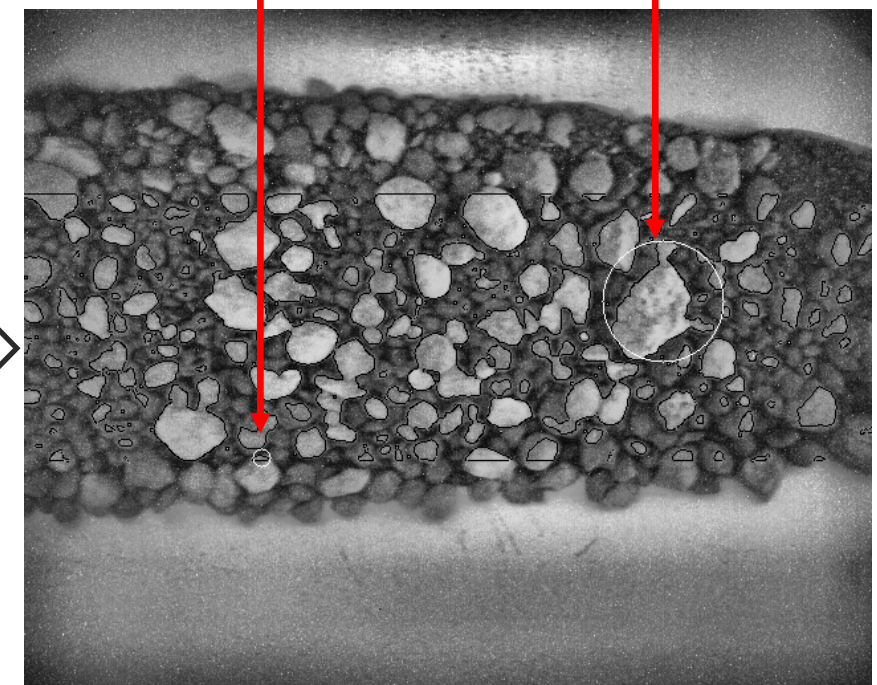
SWIR image



Binarization



Edge detection



Smallest and biggest clinker

Contours detection



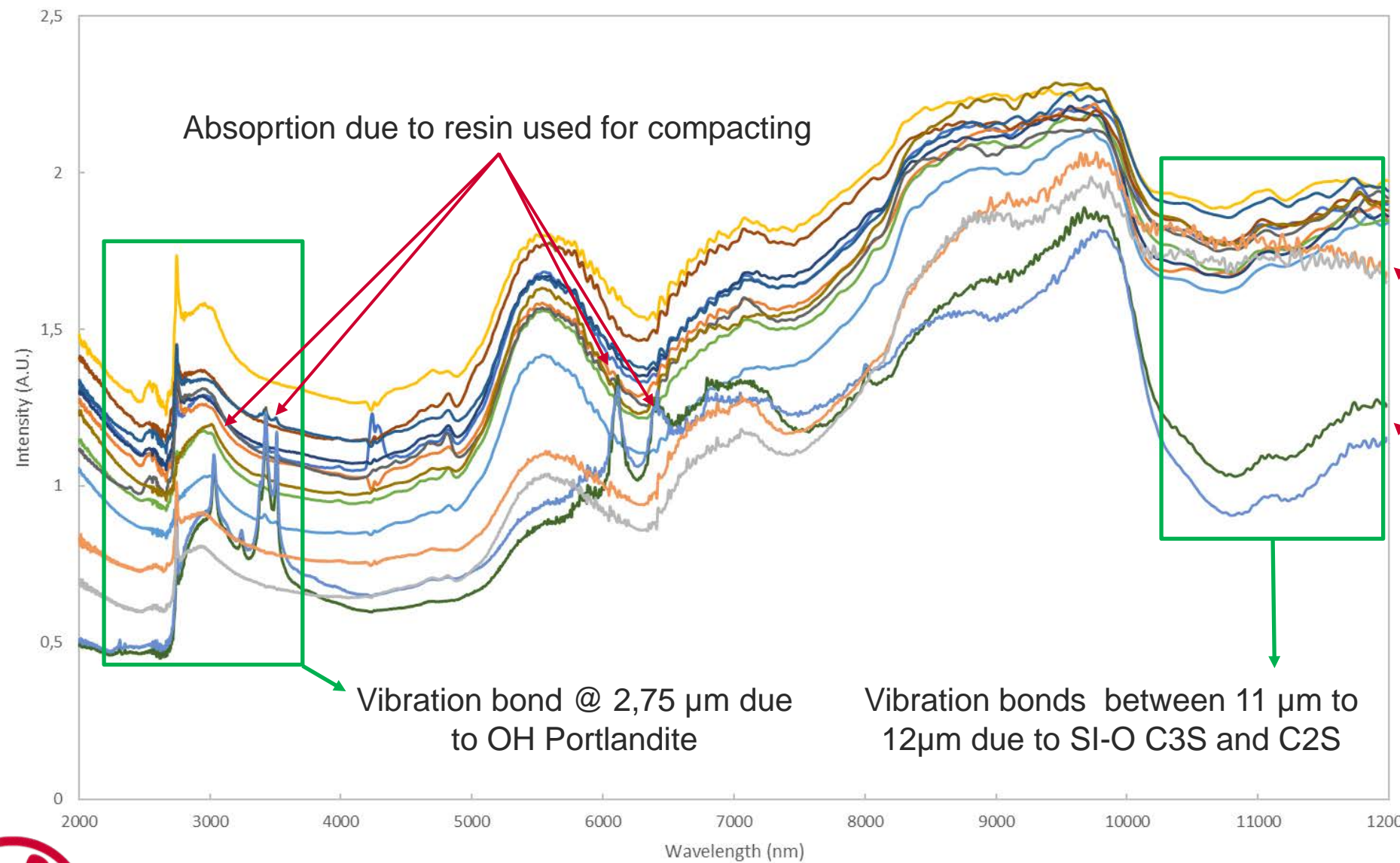
# Phase estimation: Infrared measurements

Bonds	Wavenumber (cm <sup>-1</sup> )	Wavelength (nm)	Phase/compound	CCN
Si-O	876	11415.5	Ca <sub>3</sub> SiO <sub>5</sub>	Alite (C <sub>3</sub> S)
Si-O	840 904	11904.7 11061.9	Ca <sub>2</sub> SiO <sub>4</sub>	Belite (C <sub>2</sub> S)
Al-O	700 740	14285.7 13513.5	Ca <sub>3</sub> Al <sub>2</sub> O <sub>6</sub>	Celite (C <sub>3</sub> A)
O-H	3640	2747.2	Ca(OH) <sub>2</sub>	Portlandite

Infrared vibration bonds monitored that are characteristic of CCN phase

Out of range for spectrophotometry technology used

Clinker characterization on MWIR/LWIR



Spectra obtained with clinker



Raw material.  
Dispersion due to granularity  
Sampling system complex to develop

Spectra obtained with powder



Grinded material.  
More homogeneous  
Sampling system complex to develop

Spectra obtained with tablet



Compacted material.  
More homogeneous  
Resin interference but sampling system is easier to develop

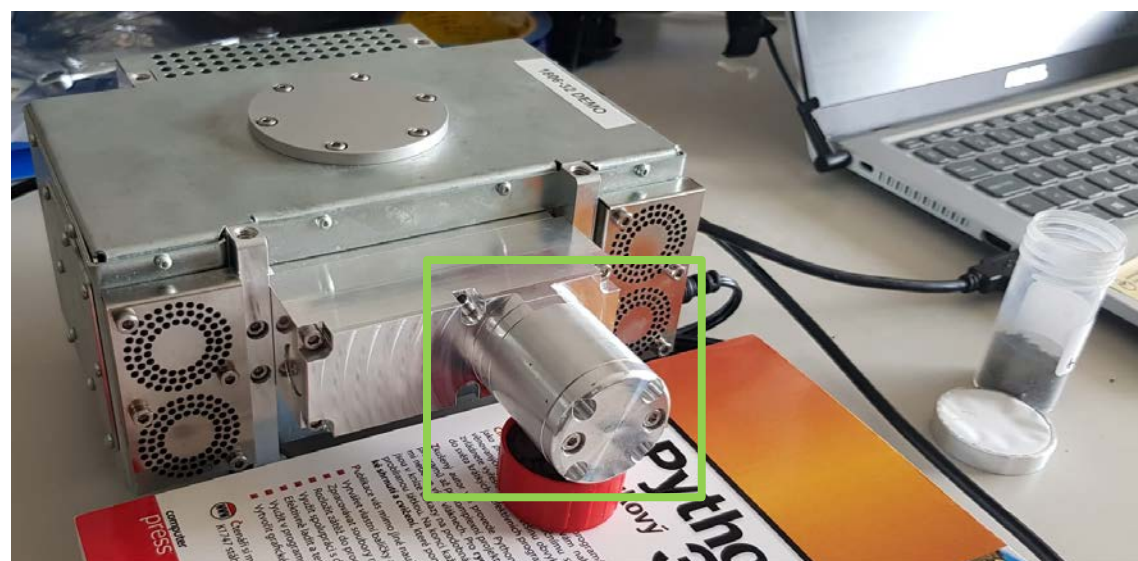
➔ Correlation established comparing with XRD/XRF measurements



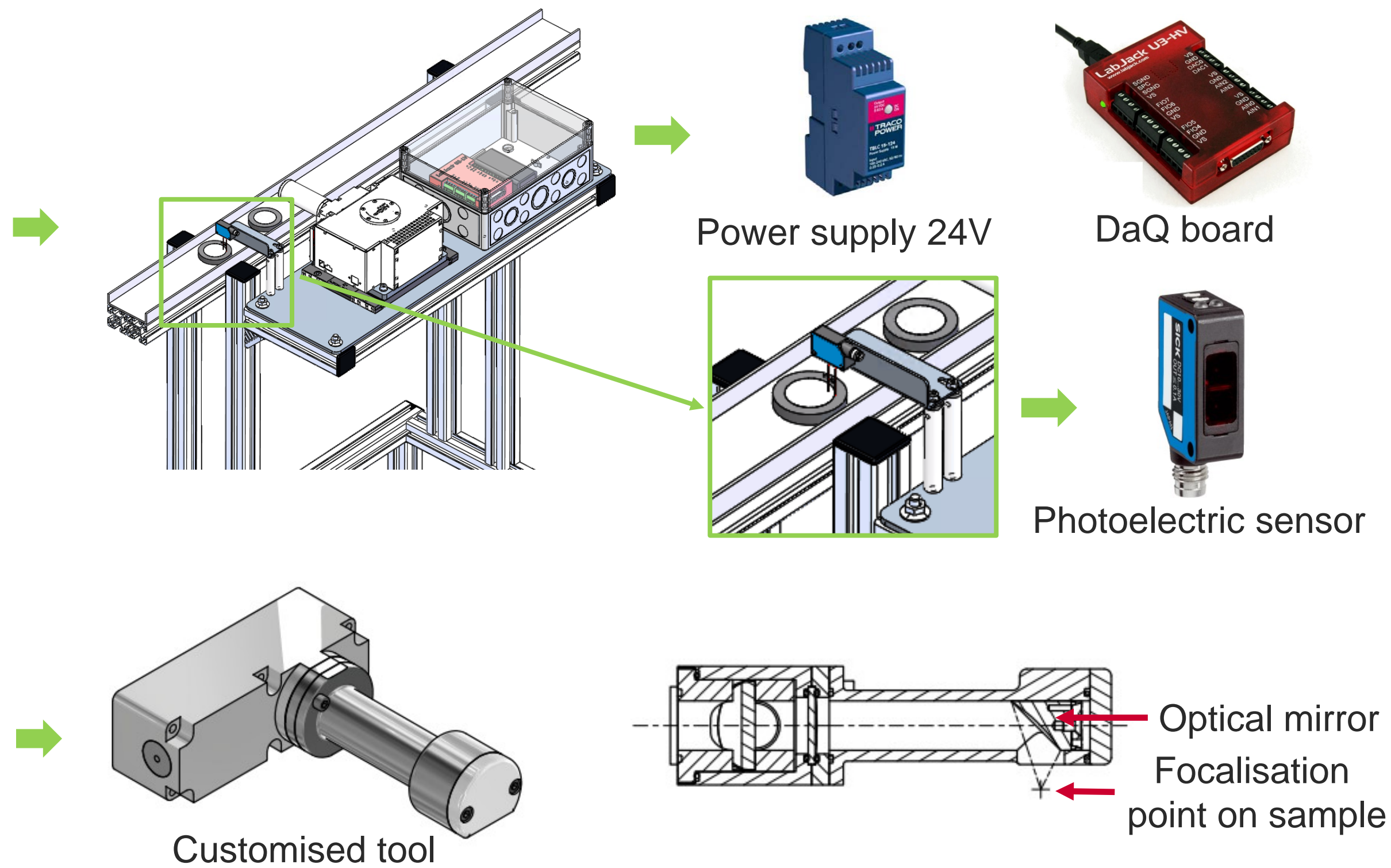
# Solution based on infrared spectrophotometry for laboratory



SECIL factory laboratory



Comon path spectrophotometer



## Next steps

### ***Integration:***

- Integrate enclosure in conveyor pipe
- Optimize transportation belt system
- Integrate spectrophotometer in laboratory
- Connect to SCADA

### ***Fine tuning and data analysis:***

- Collect data to link temperature and size measurement with clinker quality production/control
- Collect data to improve model for phase estimation



# TOWARDS MORE EFFICIENT CEMENT INDUSTRIES

ONLINE TECHNICAL WORKSHOP

1 8 0 9 2 3

1 1 : 3 0 TO 1 3  
CEST



**MAIN ACHIEVEMENTS ON CEMENT  
DEMO SITE  
Valter Tavares (SECIL)**



This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 869939.

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## SECIL Goals

To improve the plant **environmental performance** by replacing fossil fuel for alternative fuels, decreasing CO<sub>2</sub> emissions.

To increase the knowledge about the process conditions and feedstock characteristics, ending up in an **improvement of the plant efficiency** (energy, cost, process yield).

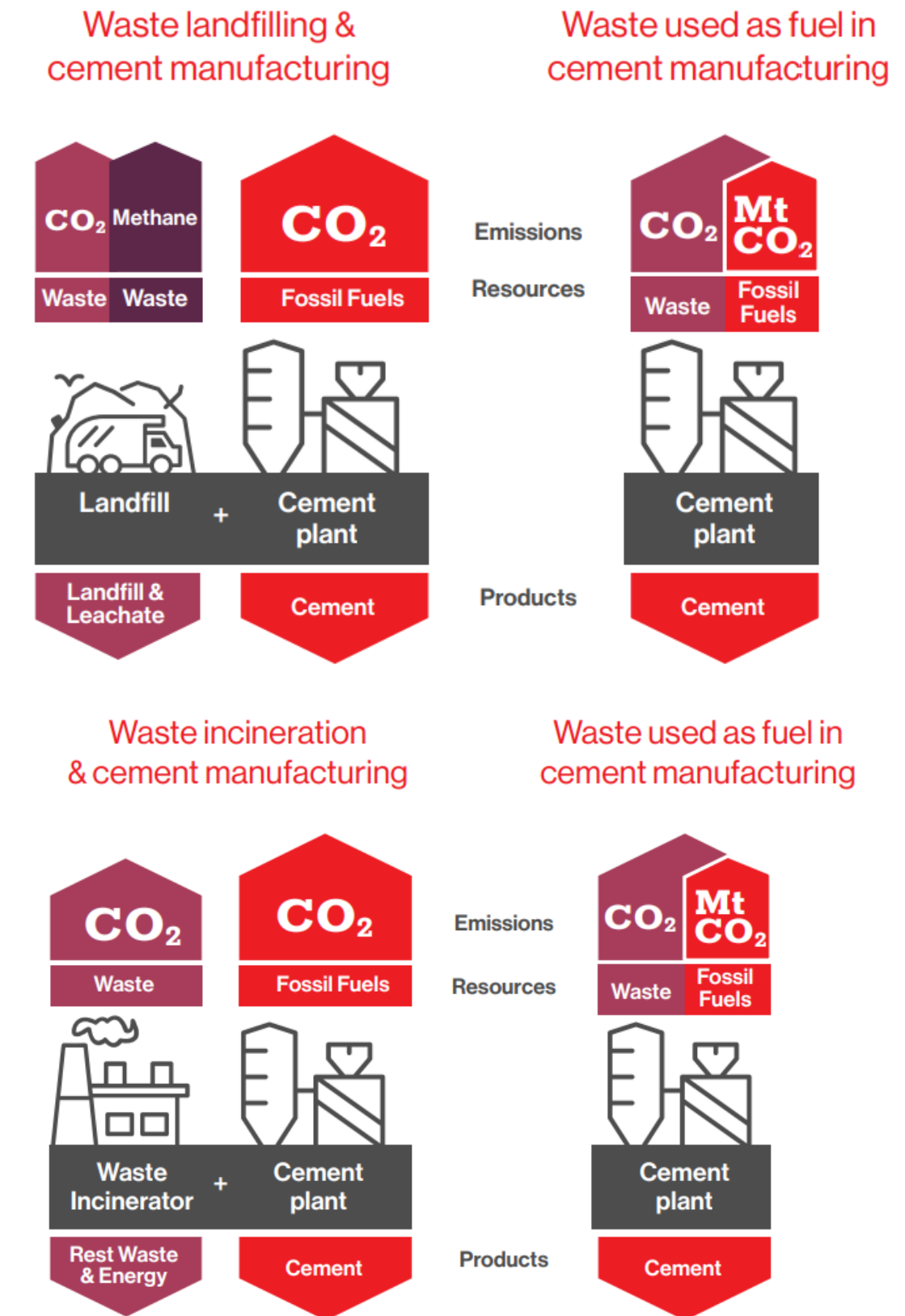


Maceira-Liz



## Why use Alternative Fuels (AF)?

- **Fuel emissions** account for approximately **35% to 40% of total CO<sub>2</sub> emissions** from cement manufacturing.
- Alternative fuels are derived from **non-primary materials (waste or by-products)** and can be biomass, fossil or mixed (fossil and biomass) alternative fuels. SECIL uses RDF (Refuse Derived Fuel) whose alternative **disposal option is incineration or landfilling**.
- The extremely high temperatures and residence times of a cement kiln ensure these are managed in a **safe and environmentally sound way**.
- **CO<sub>2</sub> is saved** by replacing fossil fuels with the alternative waste streams and through those emissions not being released by incineration or landfilling.



Source: CEMBUREAU



## RDF Challenges

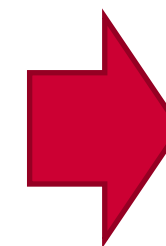
- High heterogeneity (size, material)
- High variation of calorific value
- High variation of moisture content
- Chlorine content
- Flame control
- Product quality



Cement kiln



Petroleum coke



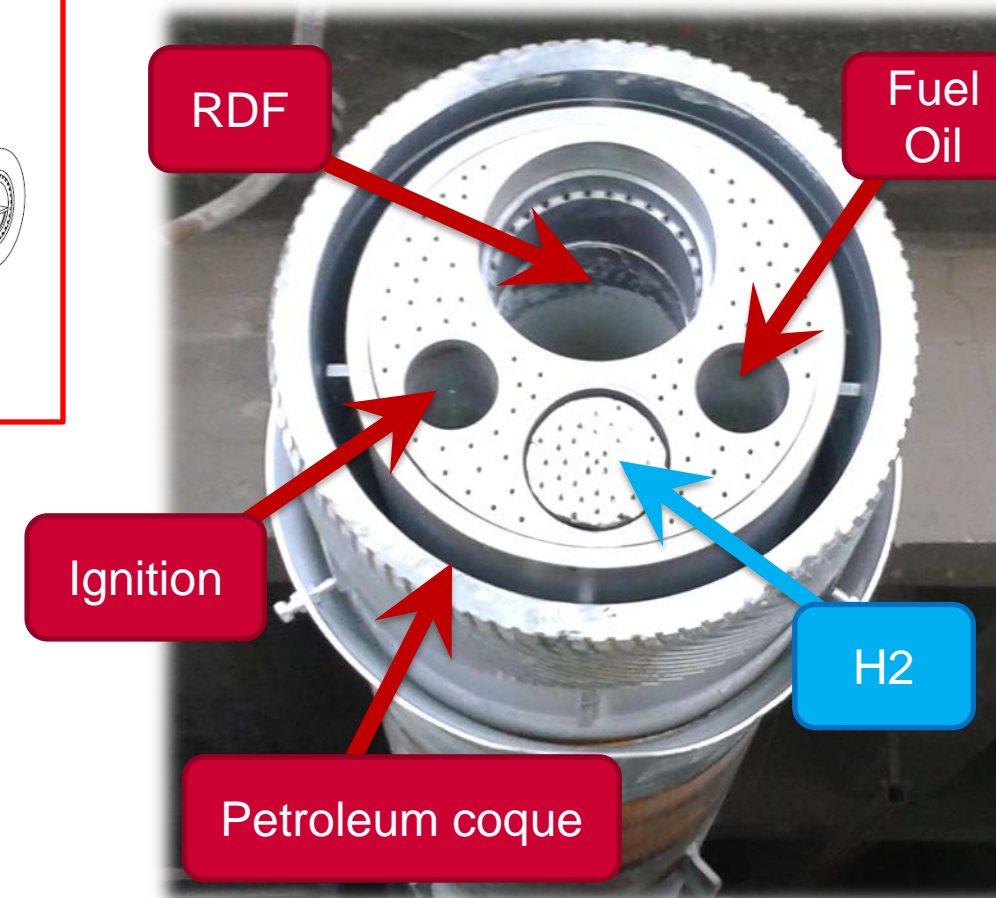
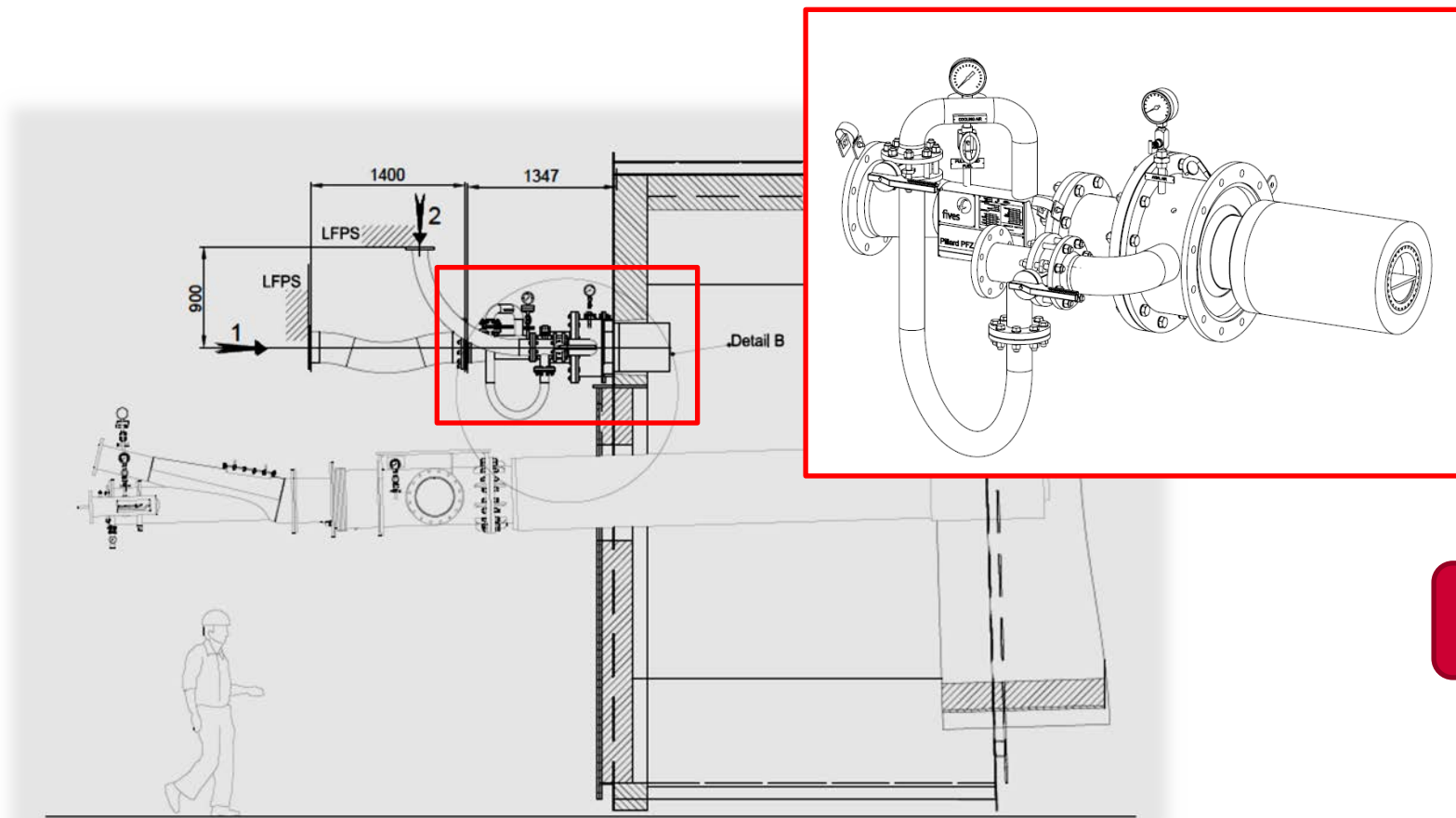
RDF (Refuse Derived Fuel)



## New burner design

Based on CFD models and trials on a prototype burner, we defined the **new design of the main burner**.

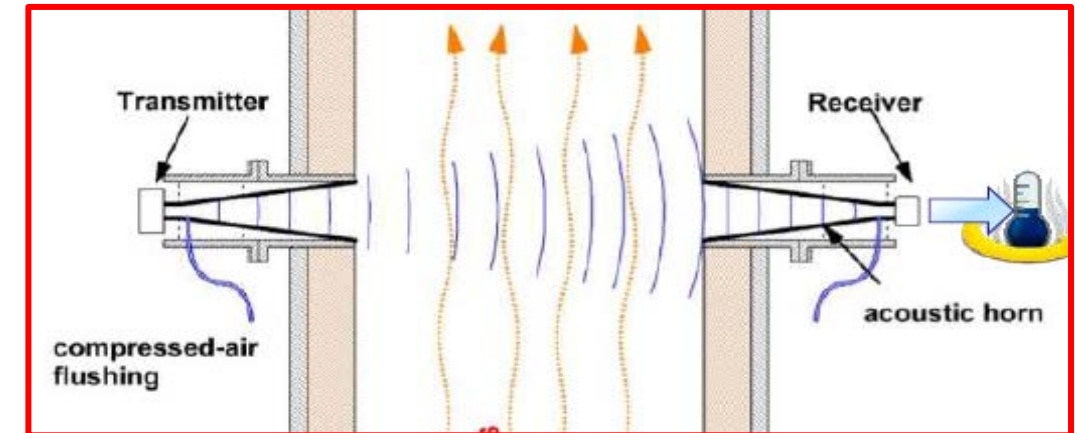
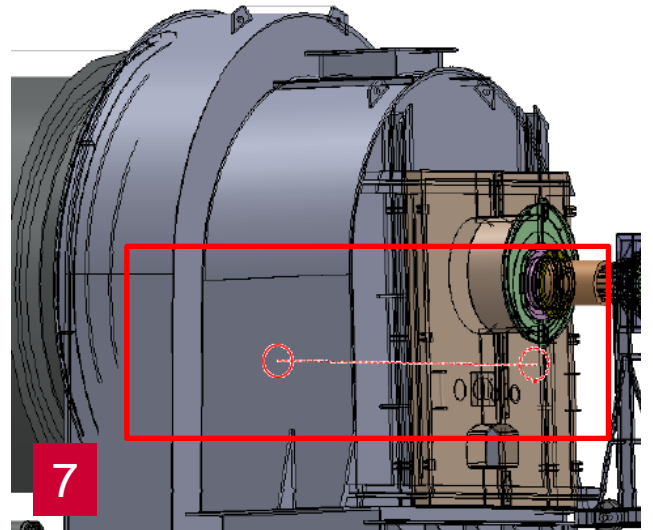
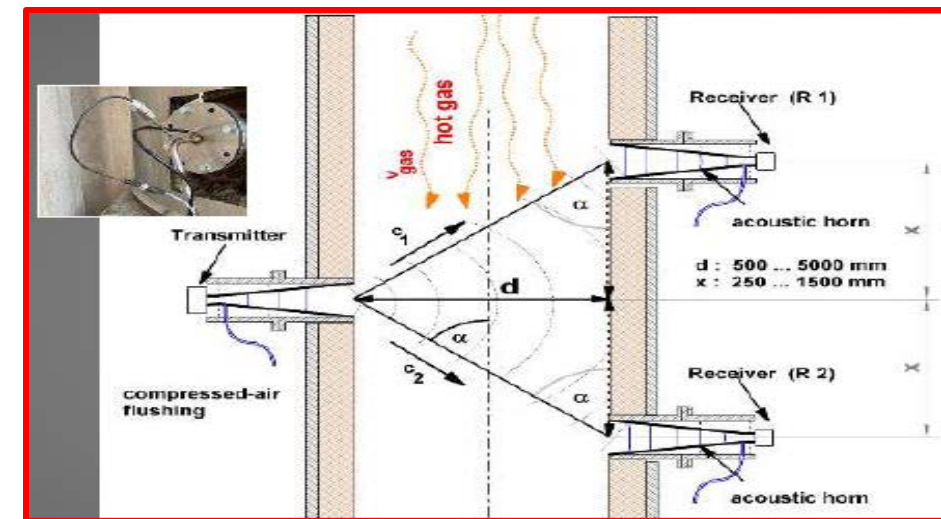
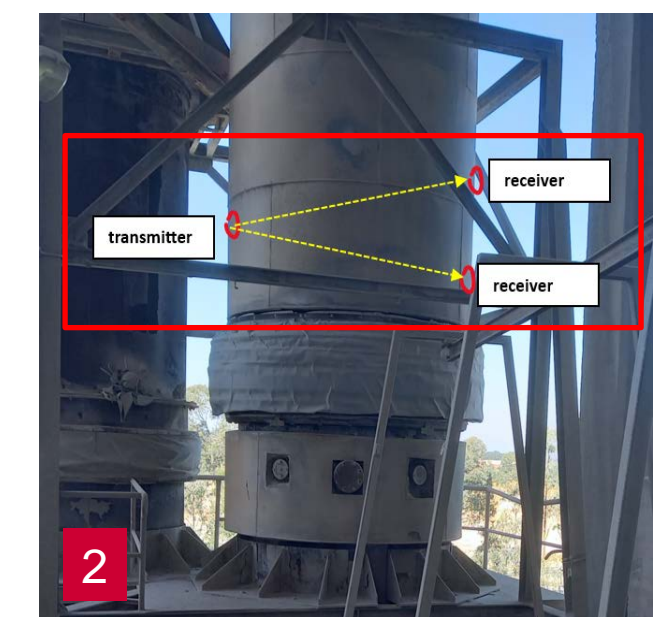
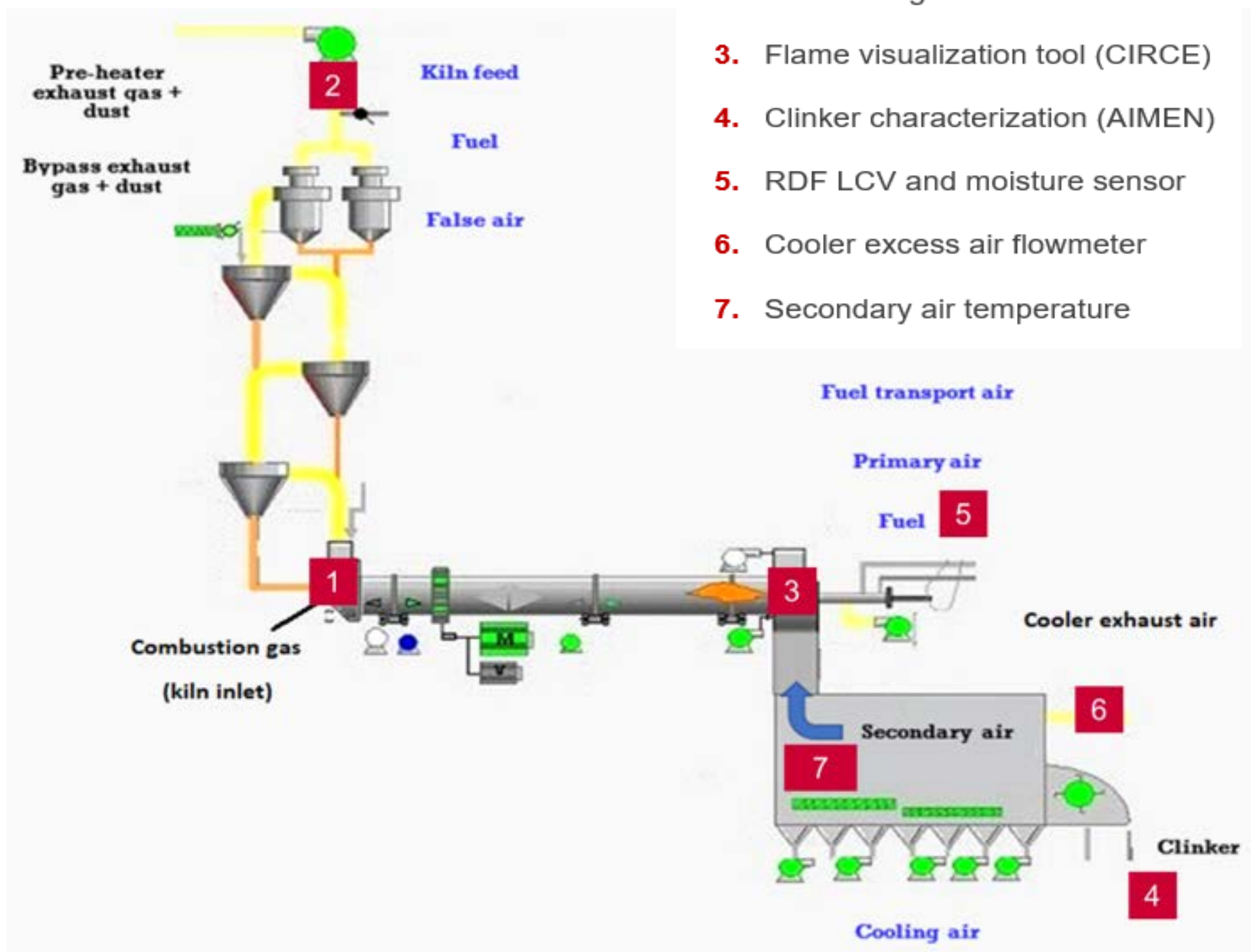
- Conclusion: Use two different RDF streams in the main burner.
- Solution: Satellite burner:
- Conclusion: Use a high calorific fuel to increase RDF rate.
- Solution: Inject H<sub>2</sub> in the main burner:





# New sensors

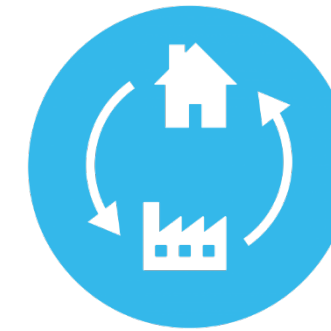
1. Kiln Inlet Gas Analyser
2. Preheater gas flowmeter
3. Flame visualization tool (CIRCE)
4. Clinker characterization (AIMEN)
5. RDF LCV and moisture sensor
6. Cooler excess air flowmeter
7. Secondary air temperature



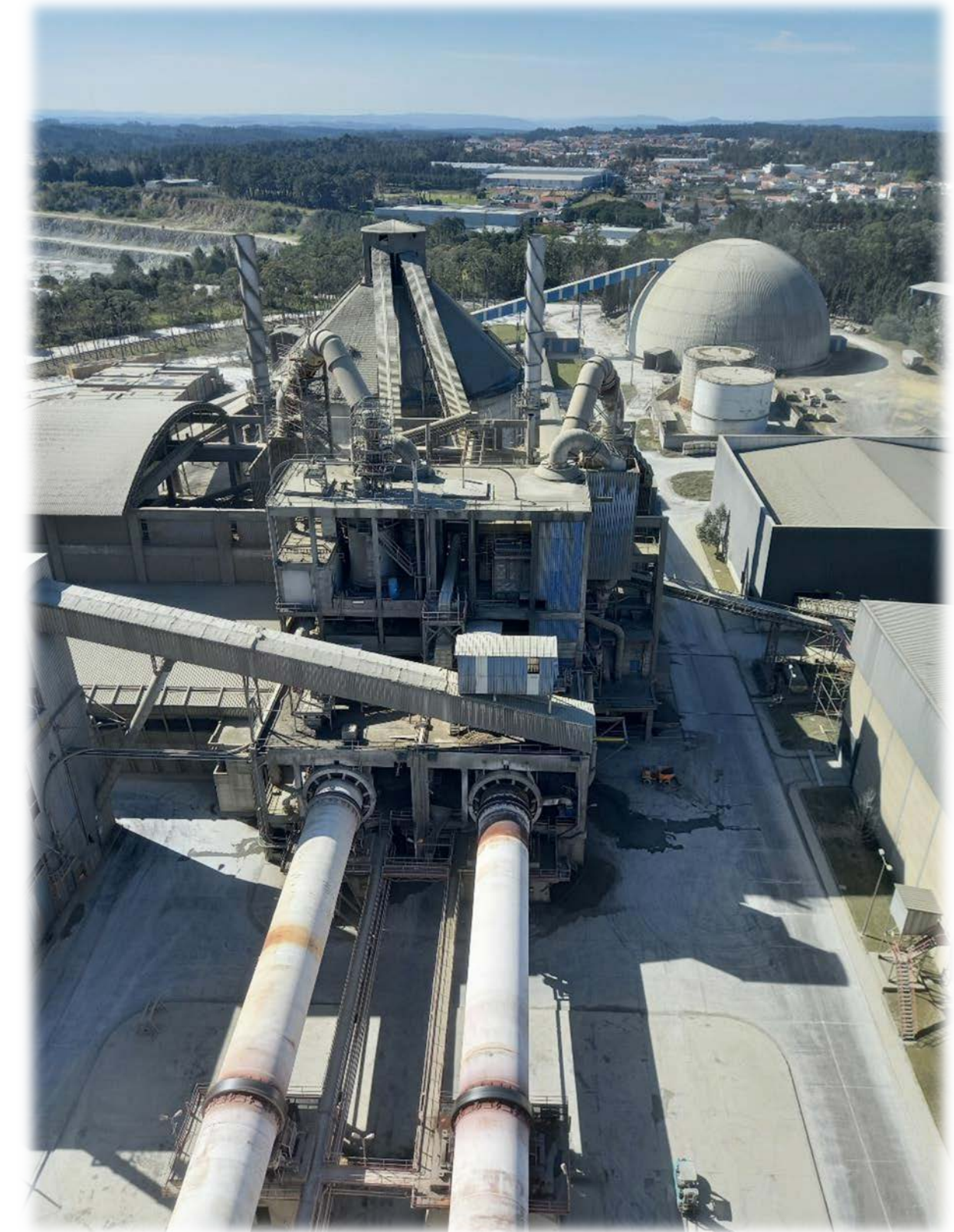


## Next Steps

- **Validation tests:**
  - New burner
  - New sensors
  - Kiln digital twin/ Decision Support System (DSS).
- **Optimization:**
  - Reduce environmental footprint
  - Reduce energy consumption
  - Improve productivity
  - Improve quality
- **Test hydrogen in the main burner**
- **Development of machine learning models**
- **Development of the SECIL replication strategy**



Circular economy



Maceira-Liz



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This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 869939.

**Q&A**  
**Olga Lysenko (IVL)**  
**Diego Redondo (CIRCE)**

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**Project coordinator**

Diego Redondo, Fundaciòn CIRCE  
[dredondo@fcirce.es](mailto:dredondo@fcirce.es)

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